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STUDY OF A FAIL-SAFE ABORT SYSTEM FOR AN ACTIVELY COOLED HYPERSONIC AIRCRAFT

— COMPUTER PROGRAM DOCUMENTATION —

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PREPARED BY:

L. A. Haas

L. A. HAAS, SR. ENGINEER THERMODYNAMICS

APPROVED BY:

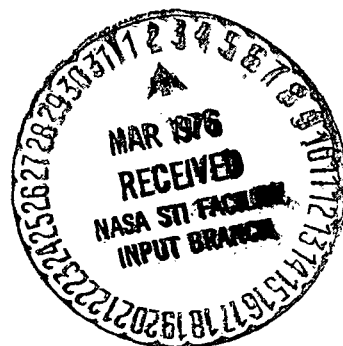
R. L. Herring

R. L. HERRING, PRINCIPAL INVESTIGATOR

APPROVED BY:

C. J. Pirrello

C. J. PIRRELLO, STUDY MANAGER



MCDONNELL AIRCRAFT COMPANY

Saint Louis, Missouri 63166 (314) 232-0232



MCDONNELL DOUGLAS

CORPORATION

ABSTRACT

This report is a user's manual for the Fail-Safe Abort System TEMPerature Analysis Program, FASTEMP. This program was used to analyze fail-safe abort systems for an actively cooled hypersonic aircraft (Contract NASA-Langley, NAS1-13631). FASTEMP analyzes the steady state or transient temperature response of a thermal model defined in rectangular, cylindrical, conical and/or spherical coordinate system. FASTEMP provides the user with a large selection of subroutines for heat transfer calculations. The various modes of heat transfer available from these subroutines are:

- o Heat storage
- o Conduction
- o Radiation
- o Heat addition or generation
- o Convection
- o Fluid flow

These modes of heat transfer can be simulated by the program in the solution of one, two, or three dimensional heat transfer problems. The modes may be modeled by rectangular, cylindrical, conical and/or spherical geometries. Any combination of modes and geometries is allowed for analysis of either transient response or steady state temperatures.

The program obtains its solution using the backward-difference method. The maximum number of nodes that may be solved depends upon the thermal model and the solution method used with an absolute maximum of 9999 nodes.

The program is written in a combination of Fortran IV and Assembler language, COMPASS, for the CDC Series 6000 and CYBER Series Computers. Minimum core requirements are 47000₈ core locations on the Scope operating system.

This report contains general information on the program and is designed to aid the engineer in setting up a problem and obtaining solutions with a fast turnaround. Program structure, solution techniques, input data and program output are discussed. A sample problem is presented and program usage is discussed. The program input/output is designed for utilization of customary engineering units.

FASTEMP

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NOMENCLATURE

<u>Symbol</u>	<u>Definition</u>
A	Area, in ²
CP	CDC Central Processor
C _p	Specific heat at Constant Pressure, Btu/lb-°R
F	Radiation View Factor
h	Heat Transfer Coefficient, Btu/hr-ft ² -°R
k	Thermal Conductivity, Btu/hr-ft-°R
\dot{m}	Mass Flow Rate, lb/hr
Ø	Stands for alphabetic letter O
Q	Heat Flux, Btu/hr
ΔT	Temperature Difference, °R
T	Temperature, °R
T _m	Boundary Temperature, °R
V	Volume, in ³
ΔX	Conduction Path Length, in
ε	Emissivity
ρ	Density, lb/ft ³
σ	Stefan-Boltzmann constant, 0.1714 x 10 ⁻⁸ , Btu/hr-ft ² -°R ⁴
b	Superscript, means leave a blank in given card column

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1. INTRODUCTION

This user's manual for the FASTEMP Heat Transfer Computer Program contains general information on program usage. The heat transfer program consists of a Thermal Analyzer (control subroutine) and user called subroutines, which are described in this user's manual. The computer code was written in Fortran IV and Assembler language (COMPASS) for the CDC 6000 and CYBER series computers. The user called subroutines are described in Appendix A.

This program was developed to analyze transient and steady state heat transfer problems. A problem is set up by defining a model which is made up of a finite number of lumped elemental volumes or nodes. Nodes are connected with the appropriate heat transfer terms. The user may model a very complex problem and is only limited by the amount of core available and solution accuracy. (Solution accuracy is discussed in Section 7.) The user may set up one, two or three dimensional problems using the following modes of heat transfer:

- o heat storage
- o conduction
- o radiation
- o convection
- o heat flux
- o fluid flow

The modes of heat transfer may be modeled with rectangular, cylindrical, conical and/or spherical geometries.

The program obtains a solution for temperatures using the backward finite difference method for the heat balance equations. This method results in a set of simultaneous equations which are solved. Several matrix solutions are available which optimize core or computer time. The maximum number of nodes (equations) in the thermal model depends on the selection of heat transfer modes and the matrix solution chosen as well as available computer core. The absolute maximum number of nodes which may be run is 9999 nodes. This limit is imposed by programming constraints using a four column field to specify node numbers.

The primary output of the computer program is a tabulation of the temperature of each node at problem times specified by the user. Additional output is printed for some heat transfer subroutines as described in Appendix A.

This user's manual is based on the program write-ups presented in References (1) and (2). The program reported herein and the referenced program are data

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compatible although operational on different computers for over nine years. Reference (2) program contains additional subroutines which allow building thermal models using phase change, aeroheating or orbital flux calculations, and other analysis oriented subroutines.

2. PROGRAM STRUCTURE

FASTEMP contains a thermal analyzer control subroutine which interfaces between the user and the computer system. The user initiates the job by compiling a subroutine (EQDAT) which calls heat transfer mode subroutines. The compiled EQDAT subroutine is loaded with the thermal analyzer controller and the library of user called subroutines and execution is initiated. The user then supplies data for the called subroutines and a model is analyzed by the program. A heat transfer problem may be analyzed using a full set of data, called a basic case, or a partial set of data which are changes to a previously run case. (Input for basic and change cases is discussed in Section 4.)

Job control language (JCL) cards are also required for each job to load and execute the program. The JCL is a function of the computer system and is not covered in this report.

After loading, the execution of the main program is initiated. The control subroutine calls the subroutine EQDAT which is required and compiled for each job. This subroutine in turn calls the subroutines needed to describe the model to be analyzed. The call establishes the order in which the subroutine data must be input to the program. An example of Subroutine EQDAT is shown below:

```
SUBROUTINE EQDAT
CALL SRA
CALL DRA
.
.
.
CALL RRA
RETURN
END
```

} Subroutines called by user

In developing an effective tool useful for analysis of both small models (less than 20 nodes) and large models (over 100 nodes), the program was structured into input, setup and computing sections.

These are designed as the M (minus), the Z (zero), and the P (plus) phases of the program as denoted by the sign of the control key. The M phase preprocesses the input data cards for a case. Error messages are written if any data cards are missing (if required), unrecognizable or in the wrong order. If the case being processed is a change case, the cards will be merged with those of the case being changed. The program has two levels of change case capability. Any number of

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change cases may be run which change the basic case. A change case may also be run which changes the most recent change case. The Z phase reads the numeric input values, performs error checks, computes constants using geometrical data and stores the data for use by the P phase. The P phase computes the heat flux terms for each node, solves the heat balance matrix for node temperatures, and controls the output of the program.

Several computer clocking points are provided in the program. The computer time at the beginning of the M phase will be printed with the message time expended = XX CP (SEC). The computer time at the end of the Z phase will be printed with the same message. At the end of a case, the clocking printed is the amount of time for the P phase (time step calculations). All clocking times are computer central processor times and are printed in seconds.

The Thermal Analyzer control subroutine uses a dynamic core allocation subroutine which allows the core requirement for the program to vary in size as a function of the size of the model being analyzed. The program prints the number of locations used by the subroutines and that remaining of the core size specified for the job at several stages in the running of a case. The printed messages are self explanatory.

The P phase is used to compute temperatures from data supplied by the user. The analysis is a time transient calculation at intervals composed of a user supplied time step schedule. A time step is processed in the following manner. The P phase calls Subroutine TIMST to calculate the time step interval from user data. Then Subroutine EQDAT is called. Subroutine EQDAT calls the heat transfer method subroutines which compute and store the matrix coefficients for each heat transfer term. Properties which are a function of node temperature are evaluated at the known temperatures at the beginning of a time step. Values which are a function of problem time are evaluated for backward finite differences at the time at the end of the time step. Subroutine SOLVE is called after the matrix coefficients have been computed and stored by Subroutine EQDAT. Subroutine SOLVE calls the matrix solution subroutine (MSOLV), and the print subroutine (PRINT). Subroutine MSOLV is called to compute the node temperatures and Subroutine PRINT is called to output the results (if requested). The computed temperatures are stored as the known temperatures for use during the next time step, the matrix locations are set to zero, the problem time is updated, and the above computations are repeated.

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3. SOLUTION METHODS

A heat transfer problem is analyzed by defining a model consisting of a finite number of nodes. The nodes or elemental volumes are considered to be isothermal at any given time during the analysis. A heat balance is written for each node using the heat transfer subroutines which are explained in Appendix A. Most of the terms in the heat balance are heat flux terms, however, some are energy terms, e.g. fluid transport terms ($\dot{m} C_p \Delta T$). In this report the term heat balance includes heat flux terms and energy terms. The heat balance for a node is not restricted to any number of terms for a given mode of heat transfer, and the heat balance for a node may be written as:

$$\Sigma Q \text{ stored} = \Sigma Q \text{ conduction} + \Sigma Q \text{ convection} + \Sigma Q \text{ radiation} + \Sigma Q \text{ misc.}$$

All terms in the equations have the units of Btu/hr. Program temperatures are in degrees Rankine internally although input of initial temperatures and output of computed temperatures may be in either Rankine or Fahrenheit at the users option. A consistent set of units is used for dimensions, e.g., lengths are input in inches and areas in square inches except where otherwise specified.

The thermal analyzer uses heat balance equations formulated for each node using the backward finite difference method (Reference (3)). A set of simultaneous equations results with coefficients stored in matrix form. The user may optionally select one of several different matrix solutions (called METHODS) to optimize the core requirements or solution time.

3.1 BACKWARD DIFFERENCE SOLUTION (METHODS 3 THROUGH 8)

The backward difference heat balance equation expresses all heat fluxes in terms of the temperatures and boundary conditions at the end of a time step. The general form of the backward difference heat balance for one node is:

$$\frac{\rho C_p V (T' - T^o)}{\Delta \tau} = \frac{kA}{\Delta X} (T'_m - T') + hA (T'_m - T') + \sigma \epsilon FA (T'^4_m - T'^4) + Q'_m$$

where T' = unknown node temperature at end of time step

T^o = known node temperature at beginning of time step

T'_m = known boundary or unknown surrounding node temperatures at the end of time step

This expression is used to represent a set of simultaneous equations, linear in T with the exception of the T^4 radiative heat flux terms. An approximate linearized term is substituted for radiative terms to allow the simultaneous solution of equations which are linear in T . (The approximation used for linearization

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is presented in Appendix B.) The backward difference equation solution is always stable. However, increasing the time step increases truncation errors in the solution and the user must tailor his time step to the boundary conditions. A general discussion of this aspect is given in Reference (3).

Thermal models produce matrices which can vary widely with respect to the connection of equations represented by the matrix coefficients. The thermal analyzer has several matrix solution methods to allow the user to specify the most efficient solution technique for a given problem. The efficiency of the specialized solutions results from reductions in computer core storage and/or running time. A brief description of methods 3, 4, 6 and 8 supplied in this program is given below.

- Method 3 - This method uses a full square matrix. Method 3 may be used for any backward difference problem, however, it will waste computer core space for many problems.
- Method 4 - This method uses a tridiagonal matrix which consists of terms on the principal diagonal and the first term on each side of the principal diagonal. This solution uses minimum computer core. This type of matrix results, for example, from a one dimensional thermal model.
- Method 6 - This method uses a K-diagonal matrix which consists of the principal diagonal terms and K terms on each side of the principal diagonal terms. The value of K (the half band-width) may be specified by the user or automatically computed by FASTEMP. FASTEMP will also determine the minimum storage for the heat balance equations and set the solution method to 6, if advantageous.
- Method 8 - This method uses the Gauss-Siedel iterative solution. The only matrix terms stored are the principal diagonal terms, nonzero off diagonal terms, and the constant terms. This solution will use a very small computer core space for many problems compared to the other methods discussed above. No computations are performed on zero off diagonal terms. The relative economy of using this solution will increase with problem size. The method is not recommended for models with zero or low mass nodes.

FASTEMP**4. PROGRAM INPUT**

The input for a FASTEMP analysis consists of three distinct types: Job Control Language (JCL) cards, subroutine specification cards, and model input data. Figure 1 shows the order of the input card groups for a job that consists of one case. Data input forms are given in Appendices A and C.

The JCL input is shown in Figure 1 as groups 1, 4 and 12. These cards are a requirement of the computer system being used. The JCL card input is not presented in this user's manual since the computer system requirements are frequently changed. The user should contact the computer support group for the current JCL input requirements.

The user is allowed to code FORTRAN subroutines for inclusion in EQDAT calls. These are input as shown in Figure 1 as group 2. Group 3 is Subroutine EQDAT which calls the heat transfer subroutines, e.g., SRA (heat storage), DRA (conduction), etc.

The model input data is shown in Figure 1 as groups 4 through 10. This data describes the model being analyzed and is explained in the remainder of this section. Group 11 is the last FASTEMP data card.

4.1 PROGRAM SPECIFICATION CARDS

FASTEMP uses a dynamic loading technique which loads into the computer core only those subroutines required for each job. The Thermal Analyzer Subprogram is called by the main program and in turn requires user coding of subroutine EQDAT.

The heat transfer method subroutines described in Appendix A must be called from Subroutine EQDAT. The subroutines supplied are independent and may be called in any order. However, the input data for the heat transfer method subroutines must be in the same order that the subroutines are called in Subroutine EQDAT. Failure to do this will cause a program error and a message to be printed. An example of Subroutine EQDAT is shown below:

<u>Card</u>	<u>Column</u>	<u>Contents</u>	
7-22		SUBROUTINE ^b EQDAT	
7-15		CALL ^b QCRA	} as many subroutine calls as required
7-14		CALL ^b SRA	
.		.	
.		.	
7-12		RETURN	
7-9		END	

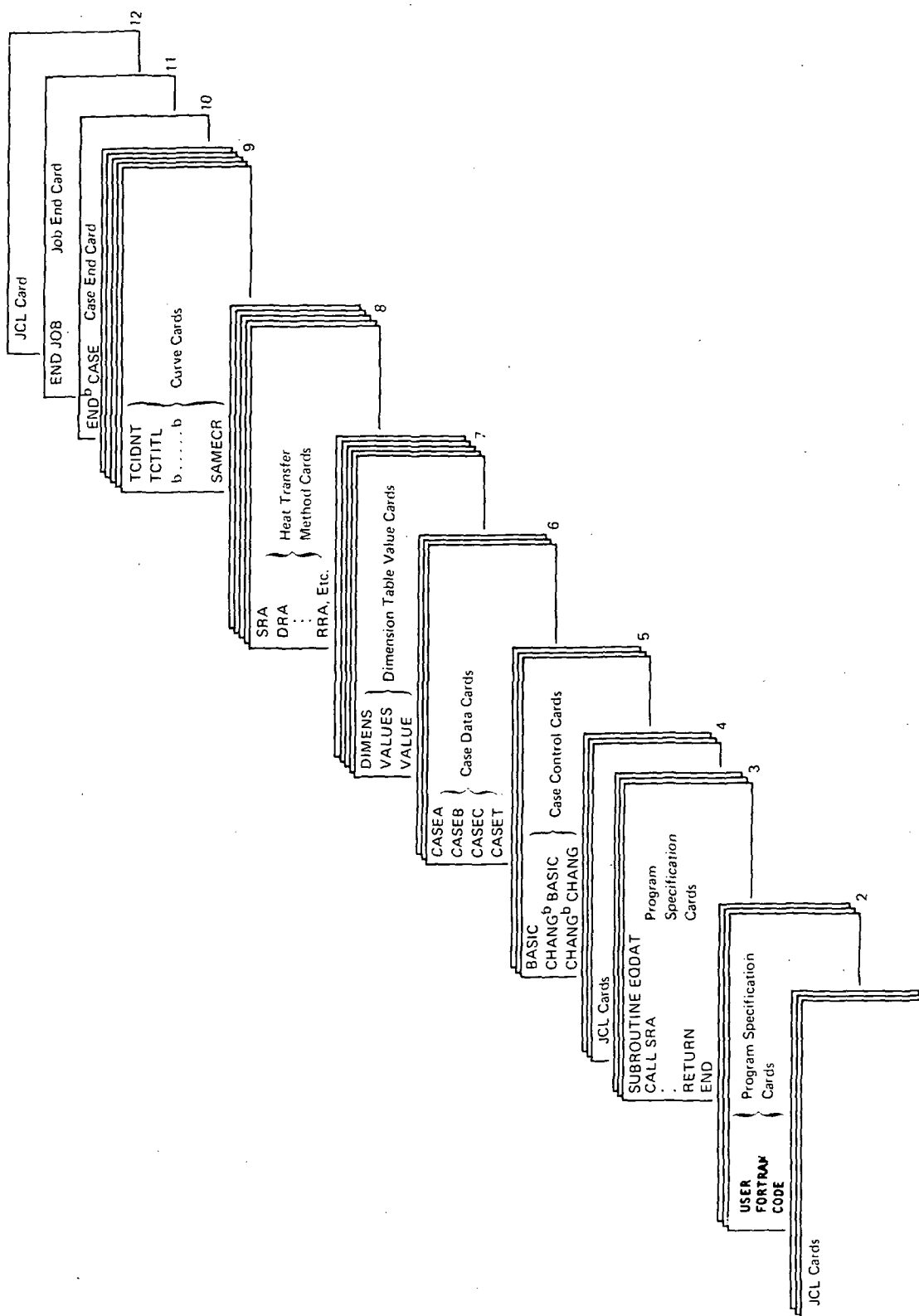


FIGURE 1 - INPUT CARD ORDER

All calls to heat transfer method subroutines start in column 7 and are standard FORTRAN cards. Heat transfer method subroutines may be called more than once in Subroutine EQDAT but they must be separated by a call to a different subroutine to correctly separate data groups. Data input format options are grouped and may be a reason for calling a subroutine more than once as explained in Section 4.4.

The card names must be punched in the card columns shown. Integer values on the case cards are indicated by a single card column number and must be right justified. Real values are designated with two card column numbers and must be punched with a decimal point and within the field shown.

4.2 CASE DATA CARDS

The CASEA card specifies a title for the case which is printed as the first line on each program output sheet. The CASEA card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEA
7-80	TITLE	User title

The CASEB card contains the alphanumeric case name, the number of nodes, a print control, an orbit control option, the solution method number, and a nonsequential node option. The CASEB data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEB
10-15	NCASE	Alphanumeric case name
20	NCA	Number of nodes
25	MPRNT	Master print control
30	NORBIT	Number of orbits
35	METHOD	Finite difference solution method
		3 - backward difference (square matrix)
		4 - backward difference (tridiagonal matrix)
		6 - backward difference (K-diagonal matrix)
		8 - backward difference (Gauss-Seidel iteration)
50	NSN	Nonsequential node option
		0 - use sequential nodes
		1 - use nonsequential nodes

The master print control may be used to suppress or to print subroutine and curve data input. MPRNT is used in conjunction with a print control on the

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subroutine and curve data cards (NPRNT). The value $1\text{MPRNT} + \text{NPRNT}$ is computed for each subroutine and each curve and the following criteria is used:

if $(\text{MPRNT} + \text{NPRNT}) > 0$ subroutine or curve data not printed

if $(\text{MPRNT} + \text{NPRNT}) \leq 0$ subroutine or curve data printed

The orbit control option, NORBIT, is used to recycle the program through the time history NORBIT times with initial temperatures continually updated. This is used primarily to simulate orbit operation but can also be used to calculate steady state conditions.

Cases may be run with either sequential or nonsequential node numbering. The sequential option requires the nodes to be numbered 1 through NCA and the node numbers and equation numbers are the same. The nonsequential node option allows node numbers of 1 through 9999 and the equation numbers (1 through NCA) are assigned in the order that the nodes are encountered in the input data.

The CASEC card contains the case beginning time, the case final time, the maximum temperature allowed, the minimum temperature allowed, the initial temperature option, a constant to be added to all initial temperatures and a solution method parameter. The CASEC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASEC
11-20	BTIME	Beginning time
21-30	FTIME	Final time
31-40	TMAX	Maximum temperature allowed ($^{\circ}\text{R}$) - any computed temperature above this value will cause termination of the case
41-50	TMIN	Minimum temperature allowed ($^{\circ}\text{R}$) - any computed temperature below this value will cause termination of the case
51-60	TEQAL	Initial temperature option if TEQAL > 0 - set all initial temperatures to TEQAL = 0 - read initial temperatures from CASEC cards < 0 - use final temperatures from preceding case as initial temperatures
61-70	ADD2T	Constant which is added to all initial temperatures

CASET cards are only required if the value for TEQAL on the CASEC card is zero. An initial temperature must be input for each node, five temperatures per card. For a sequential node case, the temperatures must be input in the order 1 through NCA. For the nonsequential use, the initial temperatures must be input in the order of the equations. The equation order is a result of the order in which the program encounters the node numbers in the user's subroutine data and care must be exercised when modeling change cases which add or remove subroutine data cards and would change code number appearance order.

A number of cases may be run serially with the final temperatures of each case used as the initial temperatures for the following case. The number of nodes in the following case must be less than or equal to the number of nodes in the preceding case. A larger number of nodes in the succeeding case will cause an error to be counted, values to be assumed for the missing temperatures and one time step to be run. Initial temperatures will be assigned using the equation order from the previous case.

The CASET data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	CASET
11-20	} TI	Initial temperature values (input in equation number order)
21-30		
31-40		
41-50		
51-60		

The case data is checked for errors, during the Z-phase, and errors may cause the following messages to be output:

- 1) number of nodes wrong
- 2) method wrong
- 3) matrix half bandwidth wrong
- 4) beginning or final time wrong
- 5) T_{\max} or T_{\min} wrong
- 6) too few CASET cards
- 7) too few temperatures from last case

Missing or incorrect data values are assumed and counted as errors. The assumed values which are used may cause or hide other errors. If errors are detected, the program will run only one time step.

4.3 DIMENSION TABLE CARDS

The dimension table is used to input values which are required by the heat transfer subroutines. The dimension table input is optional since it need not be used for heat transfer subroutines data input. (See discussion of subroutine data input - Section 4.4.) The dimension table is input by a group of cards. The first card in the group must be a DIMENS card which has the following format:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	DIMENS
10	NVAL	Number of dimension table values

The remaining cards in the group may be either VALUE or VALUES cards. The VALUE card specifies an index and one dimension table value. The VALUE data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	VALUE
10	IND	Index of Value
11-25	VAL	Value

The VALUES card specifies the value of four consecutive dimension table values. The VALUES data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	VALUES
10	IND	Index of first value
11-25	VAL1	Value IND
26-40	VAL2	Value IND+1
41-55	VAL3	Value IND+2
56-70	VAL4	Value IND+3

Dimension table values may be input in any order. If a value is input more than once, the last value specified will be used for the case. If a table value index is out of the range specified for the table, that index will extend the table by as many values as required only when $IND > NVAL$ from DIMENS card. Dimension table values which have not been defined will contain a large number (1.265×10^{322}). The card columns indicated for the number of dimension table values (NVAL) and the value index (IND) specify the right hand column of a four digit integer field, and digits in these fields must be right justified. The data card columns for the table values represent real data fields and

values in these fields should be punched with a decimal point with right justification necessary for exponent (if used).

4.4 HEAT TRANSFER METHOD SUBROUTINE CARDS

The heat transfer method subroutines are used to describe the model being analyzed. Subroutines are available to compute various modes of heat transfer, e.g., heat storage, conduction, radiation, convection, heat flux, and fluid flow. These subroutines are available with rectangular, cylindrical, conical and spherical geometries to facilitate the description of the model.

The subroutine data is input in groups of cards. One group of subroutine data is input for each subroutine in the same order that the subroutines are called in Subroutine EQDAT. A group of data input for a heat transfer method subroutine must start with a zero card number. The zero data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
14	NCARD	0
22	NPRNT	Subroutine input data print control if (NPRNT + MPRNT) > 0, input data not printed ≤ 0, input data printed
26	NFMT	Format if NFMT = 0 } general format 1 1 } 2 general format 2
30-70	IVAL	Integer data for some subroutines - 4 column fields

The subroutine name must be punched starting in card column one. All other values on this card are integer values and must be right justified in the card columns shown. The remaining cards included in the group of data input for each subroutine are input with either General Format 1 or General Format 2.

General Format 1 provides for the input of decimal data directly on the subroutine data cards. The data card format for General Format 1 is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
10	CC	Change code (See Section 4.9.3)
14	NCARD	Card number

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<u>Card Column</u>	<u>Name</u>	<u>Value</u>
18	NX1	Integer data fields
22	NX2	
26	NX3	
30	NX4	
31-40	X1	Real data fields
41-50	X2	
51-60	X3	
61-70	X4	

The subroutine name must be punched starting in column one. Integer values are indicated by a single card column number and must be right justified. Real values are designated with two card column numbers and must be punched with a decimal point within the field shown. (Any exponent is right justified.)

General Formal 2 requires the use of the dimension table described in Section 4.3. Only integer values are input on the card. Some of the integer values refer to locations in the dimension table where the decimal data is input. The data card format for General Formal 2 is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	SN	Subroutine name (SRA, DRA, etc.)
10	CC	Change code
14	NCARD	Card number
15-70	NX1-NX14	14 fields with 4 columns each

The subroutine name must be punched starting in column one. All other values on this type of card are integers and must be right justified in their data fields.

Card numbers are not required for a base case or change case; however, if individual cards are to be altered or added in a change case, card numbers must be used to identify the cards to be changed or added. No order of card numbers is required and any number of cards may use the same number. All cards with the same number are dropped in a change case, if requested.

All subroutines are available in General Format 2; however, the number of subroutines available in General Format 1 is considerably smaller. Some heat transfer method subroutines require more data input than is possible on a single card using General Formal 1.

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The use of General Format 1 has the advantage of having the numeric values on the subroutine input card where they may be easily checked. An advantage in using General Format 2 is that the same dimension table location may be used for a series of node dimensions or multipliers and changing one value in the dimension table effectively changes these values used throughout the case. A model may be set up in such a way that both general formats are desired for the same subroutines. This requires that the subroutine be called twice in Subroutine EQDAT and be separated by another data subroutine. A complete description of the heat transfer method subroutines is given in Appendix A.

The heat transfer method subroutine data is checked for errors, during the Z phase, and the following messages may be output:

- 1) Node number wrong
- 2) Node connection wrong
- 3) Subroutine references wrong dimension table value
- 4) Subroutine called had no data.

Additional information is output after the heat transfer method subroutine data has been processed in the Z phase:

- 1) A nonsequential node case will output an equation number/node number table which allows the equations to be identified. This is required to check out matrix error messages
- 2) A table listing the number of references for an equation number
- 3) A table listing the number of internodal connections for each equation
- 4) The total number of internodal connections
- 5) The maximum internodal connection band (the matrix half bandwidth)
- 6) A table listing the minimum equation number that is coupled to the equation listed
- 7) A table listing the maximum equation number that is coupled to the equation listed.

4.5 CURVE CARDS

The curves required for a case are each identified by a curve relative number (NRELN), a type (NTYPE), and a class (NCLAS). Curve relative number is generally assigned by the user, and the type and class are denoted according to the usage of the curve. Throughout this manual curves are designated by a three number system, i.e., "(NRELN, NTYPE, NCLAS)." The curves are a functional form which consists of one independent variable as a function of 0 through 2 independent variables (1 through 3 dimensional curves). The number of dimensions and the independent variables for a curve are selected by the user. All independent variable values must

be computed before a curve may be used. Commonly used curve arguments are set up automatically in the program; however, the user may specify and set up special curve arguments.

The curves required for a case may be input by two methods; same curve and temporary curve. Any required curve may be input by any method.

The same curve method specifies that the required curve be the same as another curve. Input of this second curve by temporary curve method will satisfy the input requirement for the first curve. The SAMECR data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	SAMECR
10	NRELN	Required curve relative number
14	NTYPE	Required curve type
18	NCLAS	Required curve class
30	NRELN2	Relative number of same curve
34	NTYPE2	Type of same curve
38	NCLAS2	Class of same curve

The temporary curve method inputs the required curve directly by cards. The curve is input by a set of consecutive cards. The first card must be the curve identification card (TCIDNT). This card specifies the curve identification, the curve form and other information which describes the curve. The TCIDNT data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	TCIDNT
10	NRELN	Curve relative number
14	NTYPE	Curve type
18	NCLAS	Curve class
22	--	--
26	NPRNT	Print control if (NPRNT + MPRNT) > 0, input data not printed ≤ 0, input data printed
30	NDIMN	Curve "dimension," may be values (0 to 3) (see discussion below)
34 } 42 } 38 } 46 }	NPTS _i	Number of points argument i (i = 1, 2)
	NARG _i	Argument i type (i = 1, 2)

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The second card is the curve title card (TCTITL) which is optional. The TCTITL data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	TCTITL
7-80	CT	Curve title

The remaining cards are the curve value cards. The curve value data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	Blank field
11-25	CV	Curve values
26-40		
41-55		
56-70		

For curves with a value of $NDIMN = 1$ or 0 , the dependent value is a constant, i.e., a function of no independent variable. The constant value is input in the second data field of the value card as shown in Figure 2A.

Curves which are a function of one independent variable, $y = f(x)$, have a value of $NDIMN = 2$. The $NDIMN = 2$ option is a curve which is interpolated linearly between points. The curve values are input with two point pairs per card as shown in Figure 2B.

All curves with multiple independent variables must be input with a regular grid, e.g., an $NDIMN = 3$ curve is represented as $y = f(x,z)$ and the sets of x values must be the same for all values of z . The three dimensional curve values are input in the following manner: 1) starting on the first curve value card, the values for independent variable one are input in ascending order, four per card; 2) starting on a new card, the values for independent variable two are input in ascending order four values per card; 3) starting on a new card, the values for the dependent variable are input in the order of all values for the second independent variable are input in the order of the first independent variable, all values for the second independent variable and the second value of the first independent variable, etc. An example of the input for a three dimensional curve is shown in Figure 2C.

During the loading of a curve, extensive checks are made. Any errors which are detected are written on the output. These messages consist of the following:

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- 1) A curve has an invalid identification
- 2) A curve has been input which is not required
- 3) A curve has been input more than once
- 4) The same curve requested is missing
- 5) A curve has an invalid dimension
- 6) A curve has an incorrect number of values
- 7) A curve has incorrect arguments
- 8) A curve has independent variables which are not in ascending order
- 9) A curve requested is missing.

If any errors are detected, an error message is written specifying that the curve has been rejected.

The card columns for the data fields of the SAMECR and TCIDNT cards specify the right hand card column of a four digit integer field. The data values must be right justified in these fields. The card columns for the curve value cards specify a real data field. These values should be punched with a decimal point with any exponent right justified.

The user must specify the arguments used to perform a table lookup. The independent variable arguments are specified on the TCIDNT card. The following commonly used argument numbers are specified by the program:

<u>Argument Number</u>	<u>Argument</u>
1	Time
	Method 3 through 8 - end of time step
2	Temperature (can be the temperature of a node or other values - see heat transfer method subroutine writeups in Appendix A).
650+NN	Temperature of Equation NN.

Other arguments are automatically computed for the heat transfer method subroutines and these arguments are defined in the subroutine writeups (Appendix A). The user may set up arguments for a specific use, e.g., altitude, velocity, Mach number, etc., by using Subroutine Curves (see Appendix A). It is recommended that special arguments be limited to argument numbers 11 through 19 to avoid conflict with built-in curve arguments.

Two curves are always required for a case: 1) the calculation interval or time step curve (1, 10, 1), and 2) the print interval for outputting results (1, 10, 2). The input of these curves may be satisfied by either of the two methods of inputting a curve, i.e., temporary curves or same curves.

[illegible]

FIGURE 2A - SAMPLE CURVE INPUT FOR NDIMN = 1

FIGURE 2B - SAMPLE CURVE INPUT FOR NDIMN = 2

FIGURE 2C - SAMPLE CURVE INPUT FOR NDIMN = 3

4.6 CASE END CARD

A case end card should be the last card in each case. The case end data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-8	CN	END ^b CASE

4.7 COMMENT CARDS

Comment cards may be placed anywhere in the user's data for convenience in identifying data. These cards will not appear in the subroutine output and are only printed out by the input sorting section. The comment data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	*
7-80	CMTT	User's comments

4.8 MULTIPLE AND CHANGE CASE CONTROL CARDS

The program provides for multiple cases to be run in a single job submittal. The first case run is assumed to be a BASIC case and no BASIC card is needed. Parametric analyses may be run by inputting a BASIC case and then running several change cases which vary desired parameters. Three types of cases may be run after the first base case, i.e., a BASIC case, a CHANG^bBASIC, and a CHANG^bCHANG case. These cards immediately follow the END^bCASE card of the preceding case.

4.8.1 Basic Card - The BASIC case control card is used to input a full set of data which is independent from any previously run case. The BASIC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-5	CN	BASIC

4.8.2 Change Basic Card - The CHANG^bBASIC case control card must be used to input changes to a BASIC case. The changes inserted for this change case always modify the last BASIC case which was input. The CHANG^bBASIC data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-11	CN	CHANG ^b BASIC

4.8.3 Change Change Card - The CHANG^bCHANG case control card must be used to input changes to the last change case which was input. A CHANG^bCHANG case may be used after a CHANG^bBASIC case or CHANG^bCHANG case. The CHANG^bCHANG data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-11	CN	CHANG ^b CHANG

4.9 CHANGE CASE DATA CARDS

Change cases may input data to modify any of the case input in groups 6, 7, 8, and 9 of Figure 1. Heat transfer method subroutines which were not called in Subroutine EQDAT cannot be added in a change case. The input data card groups for a change case must be input in the same order as the base case. To provide for the use of a subroutine which is not required in the base case, a call to that subroutine may be inserted in Subroutine EQDAT, and only a zero card input in the proper order in the base case. Data cards for that subroutine may then be added in the change case. The restriction of using only those subroutines called in Subroutine EQDAT applies to all cases which are input for a job submittal.

4.9.1 Case Data Changes - Any of the case data cards may be altered in a change case by inputting the new case card in the change case. Any card not present in the change case data will be taken from the base case. All CASET cards as well as a CASEC card must be input in a change case if any of the initial temperature values are to be changed by CASET cards.

4.9.2 Dimension Table Changes - Any of the dimension table data may be changed in a change case. The number of values in the dimension table may be increased or decreased in size in a change case. Dimension table values may be input with either the VALUES or VALUE cards. The change case cards are merged after the dimension table values from the base data, therefore values input in the change case will replace values from the base case.

4.9.3 Heat Transfer Subroutine Changes - Any of the data for the heat transfer method subroutines may be changed. Temperature nodes may be added or deleted or the data for base nodes may be changed. The changes input for a change case are merged with the base case data using the change code in column 10 and card numbers in column 14. The change code is ignored in a BASIC case. There are four change options available which have the following change codes.

<u>Change Code</u>	<u>Function</u>
X	The change code X will delete all cards for a subroutine and must be input on a zero card in the change case input.
R	The change code R indicates that the card(s) from the base case will be replaced by the card input in the change case. For this option the card number must be nonzero.

<u>Change Code</u>	<u>Function</u>
D	The change code D indicates that the card(s) from the base case with the proper card number will be deleted from the change case.
"blank"	The blank (and other characters not noted above) change code field will add the card from the change case input.

Change cards for the heat transfer method subroutines must be input in the same general format as those in the base case unless a new zero card (using X for change code) is input to change the format. Change cards may be input in any order in subroutine data cards with the exception of the zero card, which must be the first card if it is changed.

4.9.4 Curves Changes - Curves input as change case data may either be added to the change case or may replace curves in the base case. No provision is allowed for deleting a curve and it will be labeled as a curve which is not required, if it was replaced. A complete curve must be input for temporary curves, i.e., the TCIDNT, TCTITL and all value cards. No provision is made for changing individual values in a curve.

4.10 JOB END CARD

The last card in a job submittal is the ENDJOB card. This card informs the program that the last case has been read. The ENDJOB data card format is:

<u>Card Column</u>	<u>Name</u>	<u>Value</u>
1-6	CN	ENDJOB

5. PROGRAM OUTPUT

The output of the Thermal Analyzer Subroutine consists of three types of information: 1) output of the input data; 2) output of the results; and 3) output of error and warning messages. Most of the output of the input data is optional as specified by the user. The method of controlling the output of input data is discussed in Section 4. Output of the program contains some sections which are always printed, however, the majority of the output of the results of a case is under the user's control (e.g. node temperatures may be output at any problem time). Output of node temperatures is controlled by the print interval curve (1, 10, 2). Error messages are output specifying incorrect input data. Errors found in the input data cause the program to compute one time step only and to terminate the case. (See Section 7 for an explanation of the procedure used.)

The first page of output gives the computer time at the beginning of the M-phase and the number of core locations available for storing the data for the case and the matrix.

The next page of output for each case gives the computer time at the start of the case, the date, and the subroutines called by Subroutines EQDAT and SØLVE which require input data. Cards which have been rejected in the M-phase processing are also printed on this page (see Section 2). This output is continued on succeeding pages as required.

The next page of output gives the case specification data from the CASEB and CASEC data cards. The title from the CASEA card and the case name from the CASEB card replace the standard page header title and case name on this page and all following pages of output. Any errors in the case data will cause messages to be printed on this page of output.

The next page of output gives the dimension table if one is used. Any undefined dimension table values will contain the number 1.265×10^{322} .

The next output from the program is the input data for the heat transfer method subroutines called by Subroutines EQDAT and SØLVE. This output is optional and the user may specify individually which subroutine data will be printed. The output for each subroutine starts on a new page and continues on subsequent pages as required. Errors in the heat transfer method subroutine input data will cause messages to be printed on the output immediately after the card containing the error is processed. Any CDC hardware error codes occur for the next card which is not printed prior to error and should be noted when debugging jobs.

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Following the processing of the heat transfer subroutine data in the Z-phase, several tables are output which contain information about the heat balance matrix. If a nonsequential node number case is input, a table is output of node numbers versus equation number. Tables are output which give: the number of times each node number is referenced by a heat transfer method subroutine; the number of internodal connections for each node; and the total number of internodal connections. The maximum internodal connection band or matrix half bandwidth is also output. Two tables are printed which contain the minimum and maximum equation that a given equation has connections in the thermal model.

The next section of the output is the curve input data. This output is also optional and the curve data printed may be specified by the user. Same curve messages are output with the temporary curve data. Error messages will be output for curves which are incorrect and have been rejected.

After the curve data output, two messages are output giving the number of locations available before and after the core was requested for the matrix. The time used to the beginning of the P-phase is also output.

The results of the problem solution may be output as specified by the user. The temperatures for each node may be output at any problem time. Some heat transfer subroutines have additional output which, if desired, is printed at each computed time step. Tables of maximum and minimum temperatures for each node and the problem times for which they were computed are output after the last time step is computed.

The next page of output gives the P-phase computer time elapsed for the case, the number of time steps computed and the number of errors detected. This is normally the last page of output for a case.

6. SAMPLE PROBLEM

The sample problem presented in this section illustrates the setup of a model for a typical heat transfer problem. The sample problem does not contain all of the possible combinations of program options which are available, however, enough of the options are used to allow the user to gain a familiarity with the general setup of the deck.

The sample problem is a three dimensional heat transfer analysis which has both steady state and transient computations. Modes of heat transfer considered include heat storage, conduction, radiation, convection, and interface conductance.

The model used in this analysis is shown on Figure 3. It consists of a symmetrical section of the lower insulated surface of an actively cooled hypersonic aircraft external skin panel. Aerodynamic heat transfer through the insulated surface is absorbed by methanol/water coolant circulated through Dee-shaped tubes bonded to the inboard surface of the skin. Coolant temperature at the panel inlet was assumed to be 0°F and coolant flowrate equal to 77 lb/hr per tube. The panel skin and coolant tube were assumed to be constructed of aluminum with the back-up material of 4 lb/ft³ Johns-Manville Microfiber insulation, and the outer skin of titanium. The basic model dimensions (i.e. panel length, tube diameter, tube pitch, and material thicknesses) are shown in Figure 3, with corresponding node number identifications. A total of 208 nodes was used. The nonsequential node numbering option was used, which allows identification of different materials or sections of the model with groups of node numbers.

All nodes of the model are three-dimensional and are described by rectangular geometry, with the exception of those for the coolant within the tube, which are defined by cylindrical geometry. Nodal dimensions as well as values required by the heat transfer subroutines were input on the dimension table. Figure 4 illustrates the dimension table input parameters for the sample problem. The variable terms shown on the dimension table refer to model node dimensions and coolant Reynolds number transition from laminar (Re_L) to turbulent (Re_T) flow. Use of the dimension table, as illustrated here, provides a considerable degree of flexibility for implementing model or subroutine changes.

The mission profile used for this sample problem included an initial steady state cruise condition at Mach 4.5 and an altitude of 90,000 ft. During this time flowrate through the coolant tube was maintained at 77 lbm/hr, with a panel inlet coolant temperature of 0°F. At a time of -15 seconds, a total failure of the cooling system was imposed. This was followed at a time of 0 seconds by initiation of an abort descent trajectory resulting in lower aerodynamic heating rates. It was assumed that the cooling system failure was of a nature which caused instantaneous depletion of the coolant in the tube. Aerodynamic heat transfer rates during cruise and the abort trajectory were input in terms of external surface heat transfer coefficients and adiabatic wall temperatures versus time. These were calculated separately from other analyses based on aircraft geometry and parameters of flight altitude, velocity, and angle of attack versus time. Two cases were run for the sample problem. The first case, or base case, calculated coolant and panel structure temperature distributions and coolant pressure drop during cruise prior to cooling system failure. The second case, or change case, calculated panel transient temperatures versus time from cooling system failure (-15 seconds) through the abort trajectory (600 seconds).

Initial temperatures for the base case were input for each node as an example of the CASET card input. This was not necessary for this problem since steady state equilibrium temperatures were computed by starting the case at a time of -300 seconds and computing time steps with no heat storage until time equals -15 seconds. (See Section 7 for a discussion of the method used to compute steady state temperatures.) Temperatures were computed at the calculation intervals of 30 seconds for the base case and 5 seconds for the change case as given in curve (1, 10, 1). Print output of all node temperatures is controlled by curve (1, 10, 2) and was performed at 100 second and 15 second intervals for the base case and change case, respectively. Material property values (e.g. density, specific heat, thermal conductivity, etc.) as well as interface conductance values were input in curve form either as constants or versus time or temperature. Curve inputs were also used to describe other parameters required by the heat transfer subroutines such as external surface heat transfer coefficients, adiabatic wall temperatures, coolant flowrate, coolant friction factor, etc. A total of 29 curve inputs was used for the sample problem.

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Heat storage was computed for all nodes except those of the coolant by Subroutine SRA. Conduction was computed by Subroutines DRA, DRB, and DRC. DRA was used to compute a conduction heat flux between nodes of the same material (e.g. nodes 1 and 11). DRB was used to compute a conduction heat flux between two nodes of different materials which are separated by an interface conductance (e.g. nodes 1 and 301). Subroutine DRC was used to compute conduction between two nodes of the same material which are separated by an interface conductance (e.g. nodes 1 and 101). Aerodynamic heating to the external surface (nodes 601-639) was computed by Subroutine VRA, with heat transfer coefficient and adiabatic wall temperature inputs. External radiation heat fluxes from nodes 601-639 to a 59°F sink temperature were computed by Subroutine RRA. The forced convection Subroutine VCA was used to maintain the coolant at the panel inlet (node 200) at 0°F by inputting a very high heat transfer coefficient and a 0°F adiabatic wall temperature. Subroutine FLUID B was used for the base case to compute convection heat transfer between the coolant and the tube wall as well as pressure drop down the length of the tube. Laminar flow was assumed for this case to apply below coolant Reynolds numbers of 2100, with a step change to turbulent flow at higher Reynolds numbers.

Figure 5 shows a listing of the input data cards. This listing includes the program specification cards (i.e., Subroutine EQDAT). The job control language (JCL) cards are not listed in Figure 5. Figure 6 shows the output for the sample problem. Sheets 1 through 23 show all of the output possible from the Thermal Analyzer Subprogram for this sample problem during the M and Z phases. The user may partially or totally prevent the output of the subroutine data (Sheets 5 through 15) and the curve data (Sheets 17 through 21). The remainder of the output (Sheets 24 through 28) show the output from the P phase. A change case was setup for this model as shown in Figure 5, to run the transient analysis. Figure 5 shows the method to eliminate a complete subroutine's data (X in column 10 of FLUID B card). This simulates loss of coolant fluid at -15 seconds. Only part of the output for this transient is shown.

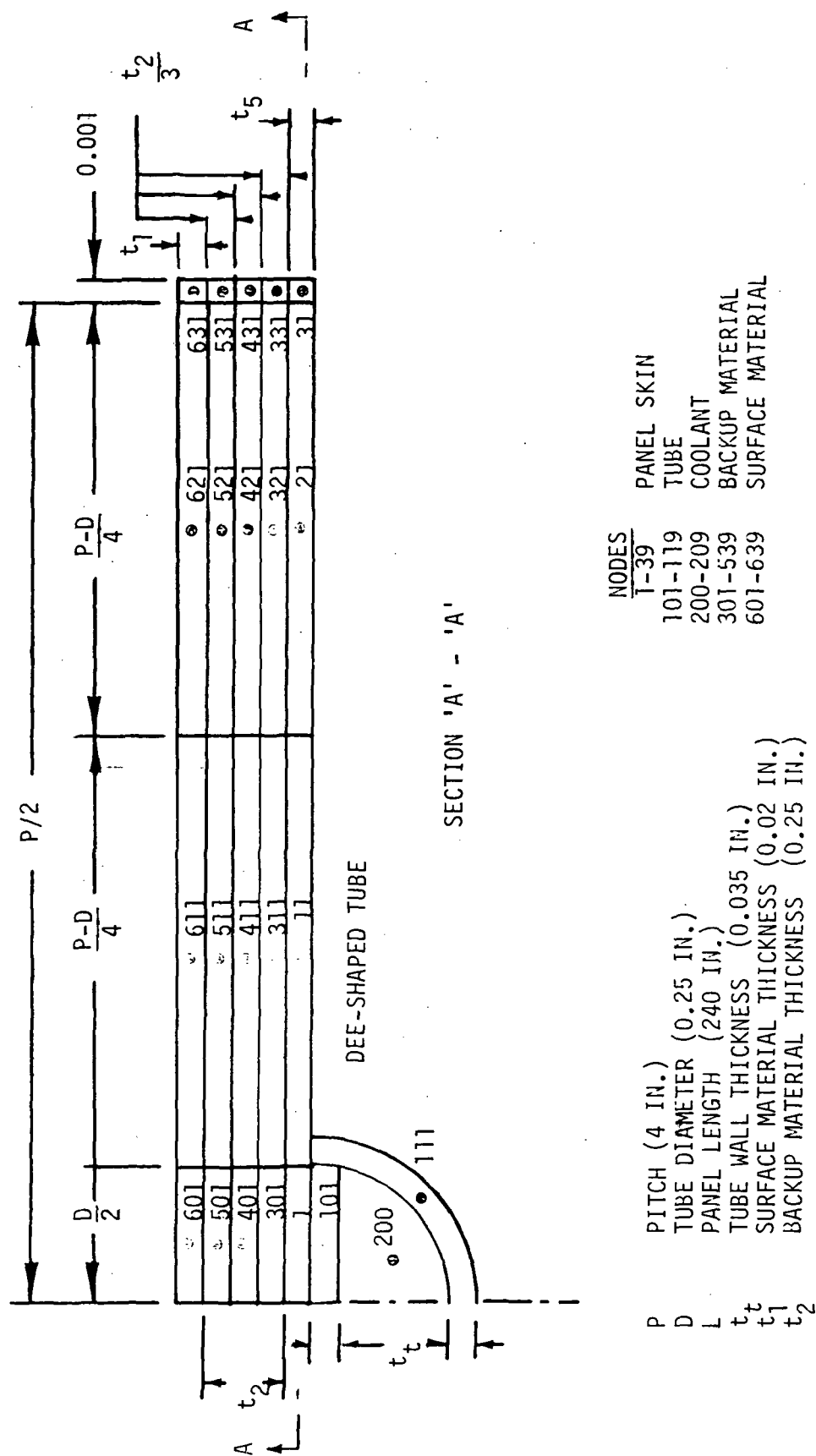


FIGURE 3 - COMPUTER PROGRAM MODEL - CROSS SECTION

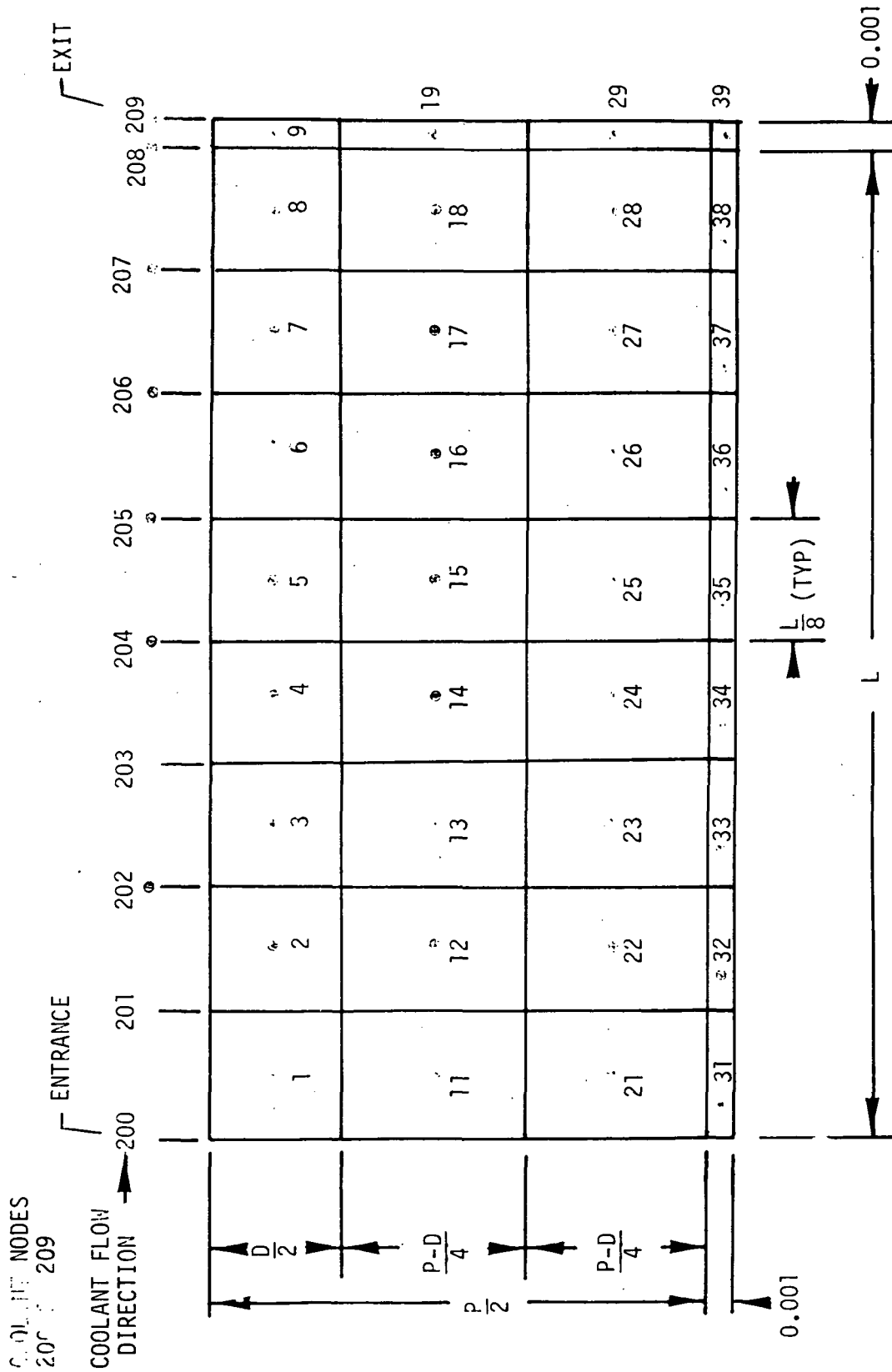


FIGURE 3A - COMPUTER PROGRAM MODEL - SECTION A-A

FASTEMP			GENERAL HEAT TRANSFER			DIMENSION TABLE INPUT 1				
1	6	NPTS 10								
DIMENS										
1	6	No. 9-10	11	25	26	40	41	55	56	70
VALUES			01	(L/8)	0.001					
		05	$(\frac{P-D}{4})$	$(\frac{D}{2})$			t_s		1.	
		09	$(\frac{L}{16}) + 0.0005$	1.			t_t		$\frac{\pi}{4} (D+t_t)$	
		13	$\frac{D}{4} + \frac{\pi}{8} (D+t_t)$	$(\frac{P-D}{8}) + 0.0005$			$(\frac{P-D}{8}) + 0.0005$		$(\frac{P-D}{4} + \frac{D}{2})/2$	
		17	90.	1.			1.		0.	
		21	Re_L	0.			0.		0.	
		25	$\frac{\pi D^2}{8}$	$Re_L \frac{L}{16}$			0.		$\frac{\pi D}{(\pi+2)}$	
		29	$1.5 (\frac{L}{8})$	$2.5 (\frac{L}{8})$			0.5		$\frac{\pi D}{4}$	
		33	$5.5 (\frac{L}{8})$	$6.5 (\frac{L}{8})$			$3.5 (\frac{L}{8})$		$4.5 (\frac{L}{8})$	
		37	t_1	t_2			$7.5 (\frac{L}{8})$		$L+0.0005$	
		41	$t_s/2$	$t_2/6$			0.3333		3.	
		45	$0.0005D$	$\frac{(P-D)L}{32}$			$t_1/2$		$\frac{D}{16}$	
		49	$\pi D^2/16$				0.0005(P-D)		0.000125L	
		53								
		57								
		61								
		65								
		69								
		73								
		77								
		81								
		85								

FIGURE 3B - COMPUTER PROGRAM MODEL - DIMENSION TABLE

SUBROUTINE EDDAT

```
CALL DRA
CALL DRB
CALL SRC
CALL VRA
CALL VCA
CALL FLUIDB
CALL RRA
CALL RETURN
END
```

[illegible]

FIGURE 4 - SAMPLE PROBLEM INPUT DATA LISTING (SHEET 1)

75.	90.	105.	120.	135.	150.	165.	180.	195.	210.	225.	240.	255.	270.	285.	300.	315.	330.	345.	360.	375.	390.	405.	420.	435.	450.	465.	480.	495.	510.	525.	540.	555.	570.	585.	600.	615.	630.	645.	660.	675.	690.	705.	720.	735.	750.	765.	780.	795.	810.	825.	840.	855.	870.	885.	900.	915.	930.	945.	960.	975.	990.	1005.	1020.	1035.	1050.	1065.	1080.	1095.	1110.	1125.	1140.	1155.	1170.	1185.	1200.	1215.	1230.	1245.	1260.	1275.	1290.	1305.	1320.	1335.	1350.	1365.	1380.	1395.	1410.	1425.	1440.	1455.	1470.	1485.	1500.	1515.	1530.	1545.	1560.	1575.	1590.	1605.	1620.	1635.	1650.	1665.	1680.	1695.	1710.	1725.	1740.	1755.	1770.	1785.	1800.	1815.	1830.	1845.	1860.	1875.	1890.	1905.	1920.	1935.	1950.	1965.	1980.	1995.	2010.	2025.	2040.	2055.	2070.	2085.	2100.	2115.	2130.	2145.	2160.	2175.	2190.	2205.	2220.	2235.	2250.	2265.	2280.	2295.	2310.	2325.	2340.	2355.	2370.	2385.	2400.	2415.	2430.	2445.	2460.	2475.	2490.	2505.	2520.	2535.	2550.	2565.	2580.	2595.	2610.	2625.	2640.	2655.	2670.	2685.	2700.	2715.	2730.	2745.	2760.	2775.	2790.	2805.	2820.	2835.	2850.	2865.	2880.	2895.	2910.	2925.	2940.	2955.	2970.	2985.	3000.	3015.	3030.	3045.	3060.	3075.	3090.	3105.	3120.	3135.	3150.	3165.	3180.	3195.	3210.	3225.	3240.	3255.	3270.	3285.	3300.	3315.	3330.	3345.	3360.	3375.	3390.	3405.	3420.	3435.	3450.	3465.	3480.	3495.	3510.	3525.	3540.	3555.	3570.	3585.	3600.	3615.	3630.	3645.	3660.	3675.	3690.	3705.	3720.	3735.	3750.	3765.	3780.	3795.	3810.	3825.	3840.	3855.	3870.	3885.	3900.	3915.	3930.	3945.	3960.	3975.	3990.	4005.	4020.	4035.	4050.	4065.	4080.	4095.	4110.	4125.	4140.	4155.	4170.	4185.	4200.	4215.	4230.	4245.	4260.	4275.	4290.	4305.	4320.	4335.	4350.	4365.	4380.	4395.	4410.	4425.	4440.	4455.	4470.	4485.	4500.	4515.	4530.	4545.	4560.	4575.	4590.	4605.	4620.	4635.	4650.	4665.	4680.	4695.	4710.	4725.	4740.	4755.	4770.	4785.	4800.	4815.	4830.	4845.	4860.	4875.	4890.	4905.	4920.	4935.	4950.	4965.	4980.	4995.	5010.	5025.	5040.	5055.	5070.	5085.	5100.	5115.	5130.	5145.	5160.	5175.	5190.	5205.	5220.	5235.	5250.	5265.	5280.	5295.	5310.	5325.	5340.	5355.	5370.	5385.	5400.	5415.	5430.	5445.	5460.	5475.	5490.	5505.	5520.	5535.	5550.	5565.	5580.	5595.	5610.	5625.	5640.	5655.	5670.	5685.	5700.	5715.	5730.	5745.	5760.	5775.	5790.	5805.	5820.	5835.	5850.	5865.	5880.	5895.	5910.	5925.	5940.	5955.	5970.	5985.	6000.	6015.	6030.	6045.	6060.	6075.	6090.	6105.	6120.	6135.	6150.	6165.	6180.	6195.	6210.	6225.	6240.	6255.	6270.	6285.
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FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 2)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 3)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA LISTING (SHEET 4)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 5)

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FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 7)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 8)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 9)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 10)

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FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 11)

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FIGURE 4 - SAMPLE PROBLEM INPUT DATA LISTING (SHEET 12)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 13)

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FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 15)

FIGURE 4 - SAMPLE PROBLEM INPUT DATA CARD LISTING (SHEET 16)

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REPORT MDC A3791

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FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 1)

SUBROUTINE EODAT
CALL DPA
CALL DPA
CALL DMC
CALL SRA
CALL VCA
CALL FLUID8
CALL DPA
RETURN
END

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FUNCTION ASSIGNMENTS
STATEMENT ASSIGNMENTS
BLOCK NAMES AND LENGTHS
- 00017
VARIABLE ASSIGNMENTS
- 00000001
START OF CONSTANTS
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START OF TEMPORARIES
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START OF INDIRECTS
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UNUSED COMPILER SPACE
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FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 2)

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FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 4)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 5)

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FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 6)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 7)

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FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 9)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 10)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 12)

HEATFAN°INS WT SWI£LD MACH 6.5L .25 IM JP INSUL .25 IN. TUDE °°75/12/00.°20.57.(1.° PAGE 11

THE FOLLOWING DATA BELONGS TO ROUTINE D23

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 13)

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 14)

CASE= MP7 SE# 1

HEATRA*INS HT SHIELD MACH 4.5LL .25 IN JM INSUL .25 IN. TUBE **75/12/08.*20.57.01.* PAGE 14

THE FOLLOWING DATA RELUNGS TO ROUTINE SPA

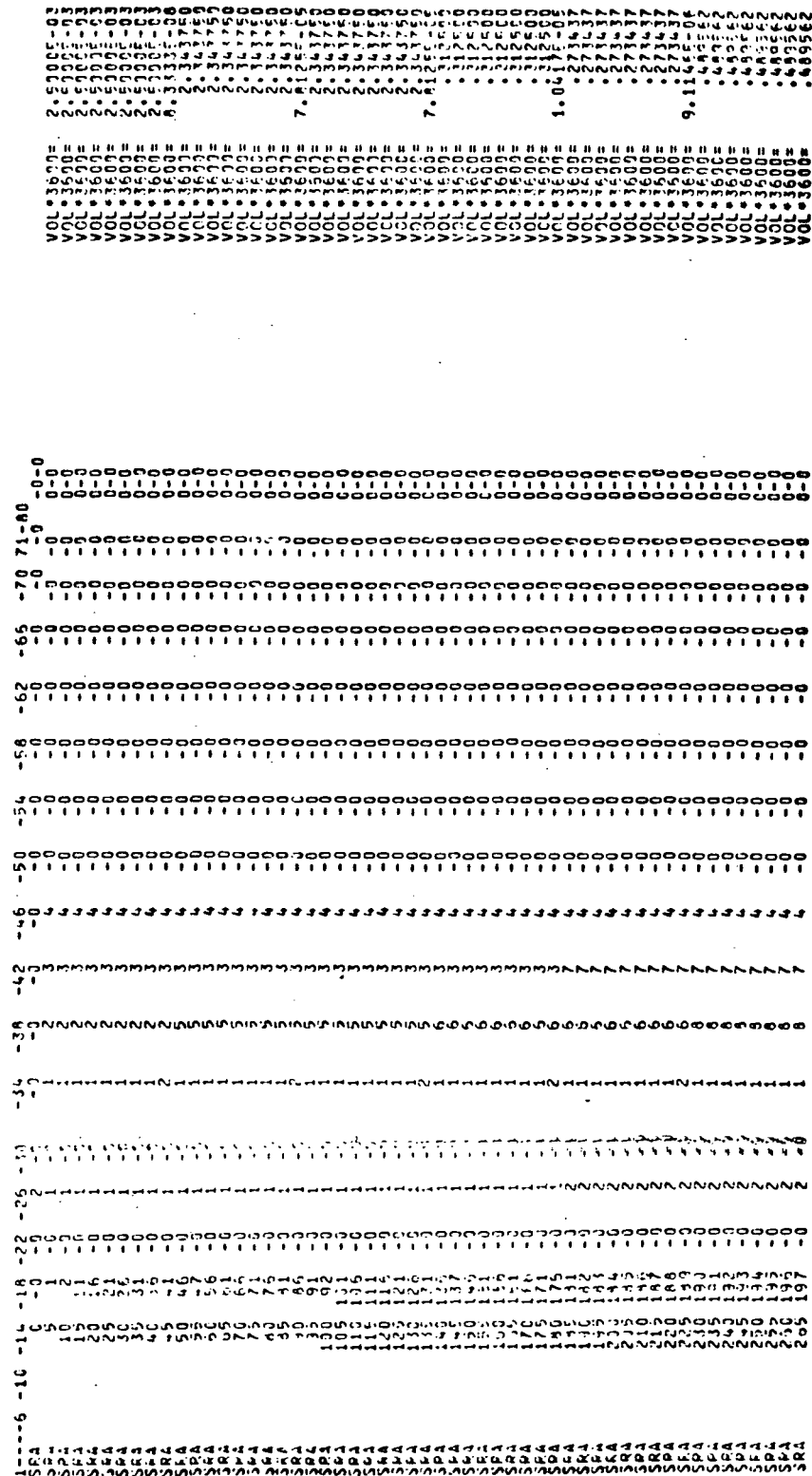


FIGURE 5 - SAMPLE PROBLEM OUTPUT. (SHEET 15)

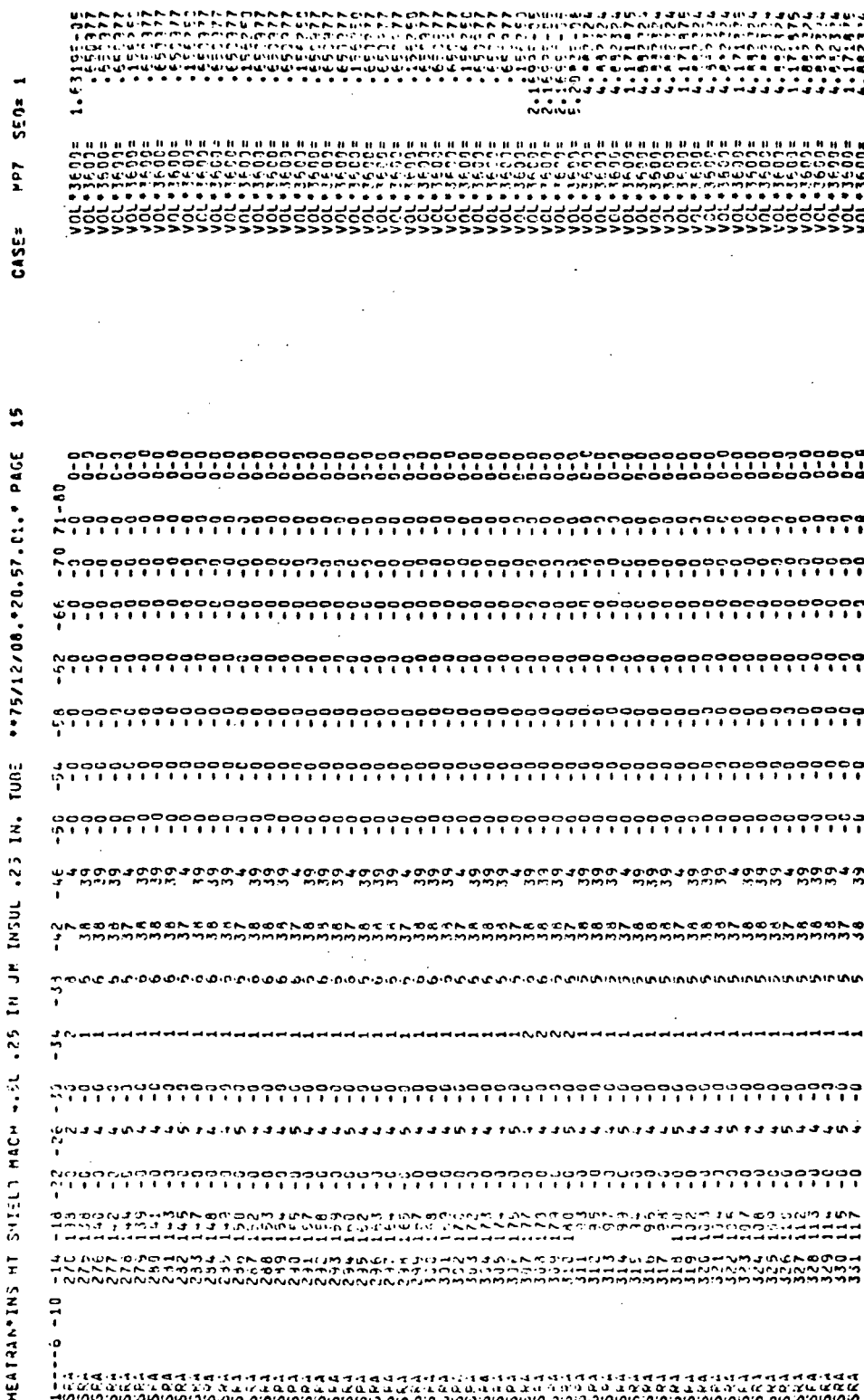


FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 16)

CASE# MP7 SEQ# 1

HEATSEAL*INS HT SHIELD MACH .25 IN. TUOE *75/12/00.*20.57.(1.* PAGE 16

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 17)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 21)

SECRET, NOFORN (73)HC 14 5010V62142H

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 22) :

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 23)

SEQUENT	VALUE	ARGUMENT	VALUE
36.000000E+01	92.200000E+00	10.600000E+02	10.700000E+01

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 24)

HEAT TRANS IN HT SHIELD MACH25 IN JM INSUL .25 IN. TURE **75/12/08.*20.57.01.* PAGE 26 CASE= MP7 SEC= 1

CURVE NO.	NAME	TYPE	VALUE	ARGUMENT	VALUE	RARG1
9	WREIN	1	20.00111111	DENSITY - FLUID - METHANOL AND WATER 6 TO 4 - THAR031174-1 HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 7	10.7000000E+01	2
10	WREIN	2	40.00011111	58.0000000E+00 56.0000000E+00 54.0000000E+00 52.0000000E+00 50.0000000E+00 SPECIFIC HEAT - FLUID - METHANOL AND WATER 6 TO 4 - THAR031174-2 HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 2	97.9000000E+00 96.0000000E+00 94.0000000E+00 92.0000000E+00 90.0000000E+00	2
11	WREIN	3	40.00011111	69.5000000E-02 THERMAL CONDUCTIVITY - FLUID - METHANOL AND WATER 6 TO 4 - THAR031174-3 HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 2	99.4000000E-02	2
12	WREIN	4	40.00011111	19.9000000E-02 VISCOSITY - FLUID - METHANOL AND WATER 6 TO 4 - THAR031174-4 HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 20	17.4000000E-02	2
13	WREIN	5	40.00011111	19.0000000E-03 JN MICRO-FIBER 4PCF INSUL DENSITY HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 4	18.3000000E-03 18.0000000E-03 17.7000000E-03 17.4000000E-03 17.1000000E-03 16.8000000E-03 16.5000000E-03 16.2000000E-03 15.9000000E-03 15.6000000E-03 15.3000000E-03 15.0000000E-03 14.7000000E-03 14.4000000E-03 14.1000000E-03 13.8000000E-03 13.5000000E-03 13.2000000E-03 12.9000000E-03 12.6000000E-03 12.3000000E-03 12.0000000E-03 11.7000000E-03 11.4000000E-03 11.1000000E-03 10.8000000E-03 10.5000000E-03 10.2000000E-03 9.9000000E-03 9.6000000E-03 9.3000000E-03 9.0000000E-03 8.7000000E-03 8.4000000E-03 8.1000000E-03 7.8000000E-03 7.5000000E-03 7.2000000E-03 6.9000000E-03 6.6000000E-03 6.3000000E-03 6.0000000E-03 5.7000000E-03 5.4000000E-03 5.1000000E-03 4.8000000E-03 4.5000000E-03 4.2000000E-03 3.9000000E-03 3.6000000E-03 3.3000000E-03 3.0000000E-03 2.7000000E-03 2.4000000E-03 2.1000000E-03 1.8000000E-03 1.5000000E-03 1.2000000E-03 0.9000000E-03 0.6000000E-03 0.3000000E-03 0.0000000E-03	1
14	WREIN	6	40.00011111	40.0000000E-01 JN MICRO-FIBER INSUL 4PCF SPECIFIC HEAT HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 6	40.0000000E-01	2
15	WREIN	7	40.00011111	18.0000000E-03 JN MICRO-FIBER INSUL 4PCF THERMAL COND. HCLAS = 0 MATRL = 0 NOIHM = 2 NPNT1 = 6	21.1000000E-03	2

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 25)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 26)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 27)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 28)

HEAT TRANS HT	SHIELD MACH	0.5L	0.25 IN	JM INSUL	0.25 IN	TUBE	0.75/1.12/0.8	0.20/0.57/0.9	PAGE	2	CASE	MP7	SEC	1
5271	6577	330	5291	560	30	5311	5321	5331	5341	5351	5361	5371	5381	5391
5272	6578	330	5292	561	33	5312	5322	5332	5342	5352	5362	5372	5382	5392
5273	6579	330	5293	562	33	5313	5323	5333	5343	5353	5363	5373	5383	5393
5274	6580	330	5294	563	33	5314	5324	5334	5344	5354	5364	5374	5384	5394
5275	6581	330	5295	564	33	5315	5325	5335	5345	5355	5365	5375	5385	5395
5276	6582	330	5296	565	33	5316	5326	5336	5346	5356	5366	5376	5386	5396
5277	6583	330	5297	566	33	5317	5327	5337	5347	5357	5367	5377	5387	5397
5278	6584	330	5298	567	33	5318	5328	5338	5348	5358	5368	5378	5388	5398
5279	6585	330	5299	568	33	5319	5329	5339	5349	5359	5369	5379	5389	5399
5280	6586	330	5300	569	33	5320	5330	5340	5350	5360	5370	5380	5390	5400
5281	6587	330	5301	570	33	5321	5331	5341	5351	5361	5371	5381	5391	5401
5282	6588	330	5302	571	33	5322	5332	5342	5352	5362	5372	5382	5392	5402
5283	6589	330	5303	572	33	5323	5333	5343	5353	5363	5373	5383	5393	5403
5284	6590	330	5304	573	33	5324	5334	5344	5354	5364	5374	5384	5394	5404
5285	6591	330	5305	574	33	5325	5335	5345	5355	5365	5375	5385	5395	5405
5286	6592	330	5306	575	33	5326	5336	5346	5356	5366	5376	5386	5396	5406
5287	6593	330	5307	576	33	5327	5337	5347	5357	5367	5377	5387	5397	5407
5288	6594	330	5308	577	33	5328	5338	5348	5358	5368	5378	5388	5398	5408
5289	6595	330	5309	578	33	5329	5339	5349	5359	5369	5379	5389	5399	5409
5290	6596	330	5310	579	33	5330	5340	5350	5360	5370	5380	5390	5400	5410
5291	6597	330	5311	580	33	5331	5341	5351	5361	5371	5381	5391	5401	5411
5292	6598	330	5312	581	33	5332	5342	5352	5362	5372	5382	5392	5402	5412
5293	6599	330	5313	582	33	5333	5343	5353	5363	5373	5383	5393	5403	5413
5294	6600	330	5314	583	33	5334	5344	5354	5364	5374	5384	5394	5404	5414
5295	6601	330	5315	584	33	5335	5345	5355	5365	5375	5385	5395	5405	5415
5296	6602	330	5316	585	33	5336	5346	5356	5366	5376	5386	5396	5406	5416
5297	6603	330	5317	586	33	5337	5347	5357	5367	5377	5387	5397	5407	5417
5298	6604	330	5318	587	33	5338	5348	5358	5368	5378	5388	5398	5408	5418
5299	6605	330	5319	588	33	5339	5349	5359	5369	5379	5389	5399	5409	5419
5300	6606	330	5320	589	33	5340	5350	5360	5370	5380	5390	5400	5410	5420
5301	6607	330	5321	590	33	5341	5351	5361	5371	5381	5391	5401	5411	5421
5302	6608	330	5322	591	33	5342	5352	5362	5372	5382	5392	5402	5412	5422
5303	6609	330	5323	592	33	5343	5353	5363	5373	5383	5393	5403	5413	5423
5304	6610	330	5324	593	33	5344	5354	5364	5374	5384	5394	5404	5414	5424
5305	6611	330	5325	594	33	5345	5355	5365	5375	5385	5395	5405	5415	5425
5306	6612	330	5326	595	33	5346	5356	5366	5376	5386	5396	5406	5416	5426
5307	6613	330	5327	596	33	5347	5357	5367	5377	5387	5397	5407	5417	5427
5308	6614	330	5328	597	33	5348	5358	5368	5378	5388	5398	5408	5418	5428
5309	6615	330	5329	598	33	5349	5359	5369	5379	5389	5399	5409	5419	5429
5310	6616	330	5330	599	33	5350	5360	5370	5380	5390	5400	5410	5420	5430
5311	6617	330	5331	600	33	5351	5361	5371	5381	5391	5401	5411	5421	5431
5312	6618	330	5332	601	33	5352	5362	5372	5382	5392	5402	5412	5422	5432
5313	6619	330	5333	602	33	5353	5363	5373	5383	5393	5403	5413	5423	5433
5314	6620	330	5334	603	33	5354	5364	5374	5384	5394	5404	5414	5424	5434
5315	6621	330	5335	604	33	5355	5365	5375	5385	5395	5405	5415	5425	5435
5316	6622	330	5336	605	33	5356	5366	5376	5386	5396	5406	5416	5426	5436
5317	6623	330	5337	606	33	5357	5367	5377	5387	5397	5407	5417	5427	5437
5318	6624	330	5338	607	33	5358	5368	5378	5388	5398	5408	5418	5428	5438
5319	6625	330	5339	608	33	5359	5369	5379	5389	5399	5409	5419	5429	5439
5320	6626	330	5340	609	33	5360	5370	5380	5390	5400	5410	5420	5430	5440
5321	6627	330	5341	610	33	5361	5371	5381	5391	5401	5411	5421	5431	5441
5322	6628	330	5342	611	33	5362	5372	5382	5392	5402	5412	5422	5432	5442
5323	6629	330	5343	612	33	5363	5373	5383	5393	5403	5413	5423	5433	5443
5324	6630	330	5344	613	33	5364	5374	5384	5394	5404	5414	5424	5434	5444
5325	6631	330	5345	614	33	5365	5375	5385	5395	5405	5415	5425	5435	5445
5326	6632	330	5346	615	33	5366	5376	5386	5396	5406	5416	5426	5436	5446
5327	6633	330	5347	616	33	5367	5377	5387	5397	5407	5417	5427	5437	5447
5328	6634	330	5348	617	33	5368	5378	5388	5398	5408	5418	5428	5438	5448
5329	6635	330	5349	618	33	5369	5379	5389	5399	5409	5419	5429	5439	5449
5330	6636	330	5350	619	33	5370	5380	5390	5400	5410	5420	5430	5440	5450
5331	6637	330	5351	620	33	5371	5381	5391	5401	5411	5421	5431	5441	5451
5332	6638	330	5352	621	33	5372	5382	5392	5402	5412	5422	5432	5442	5452
5333	6639	330	5353	622	33	5373	5383	5393	5403	5413	5423	5433	5443	5453
5334	6640	330	5354	623	33	5374	5384	5394	5404	5414	5424	5434	5444	5454
5335	6641	330	5355	624	33	5375	5385	5395	5405	5415	5425	5435	5445	5455
5336	6642	330	5356	625	33	5376	5386	5396	5406	5416	5426	5436	5446	5456
5337	6643	330	5357	626	33	5377	5387	5397	5407	5417	5427	5437	5447	5457
5338	6644	330	5358	627	33	5378	5388	5398	5408	5418	5428	5438	5448	5458
5339	6645	330	5359	628	33	5379	5389	5399	5409	5419	5429	5439	5449	5459
5340	6646	330	5360	629	33	5380	5390	5400	5410	5420	5430	5440	5450	5460
5341	6647	330	5361	630	33	5381	5391	5401	5411	5421	5431	5441	5451	5461
5342	6648	330	5362	631	33	5382	5392	5402	5412	5422	5432	5442	5452	5462
5343	6649	330	5363	632	33	5383	5393	5403	5413	5423	5433	5443	5453	5463
5344	6650	330	5364	633	33	5384	5394	5404	5414	5424	5434	5444	5454	5464
5345	6651	330	5365	634	33	5385	5395	5405	5415	5425	5435	5445	5455	5465
5346	6652	330	5366	635	33	5386	5396	5406	5416	5426	5436	5446	5456	5466
5347	6653	330	5367	636	33	5387	5397	5407	5417	5427	5437	5447	5457	5467
5348	6654	330	5368	637	33	5388	5398	5408	5418	5428	5438	5448	5458	5468
5349	6655	330	5369	638	33	5389	5399	5409	5419	5429	5439	5449	5459	5469
5350	6656	330	5370	639	33	5390	5400	5410	5420	5430	5440	5450	5460	5470
5351	6657	330	5371	640	33	5391	5401	5411	5421	5431	5441	5451	5461	5471
5352	6658	330	5372	641	33	5392	5402	5412	5422	5432	5442	5452	5462	5472
5353	6659	330	5373	642	33	5393	5403	5413	5423	5433	5443	5453	5463	5473
5354	6660	330	5374	643	33	5394	5404	5414	5424	5434	5444	5454	5464	5474
5355	6661	330	5375	644	33	5395	5405	5415	5425	5435	5445	5455	5465	5475
5356	6662	330	5376	645	33	5396	5406	5416	5426	5436	5446	5456	5466	5476
5357	6663	330	5377	646	33	5397	5407	5417	5427	5437	5447	5457	5467	5477
5358	6664	330	5378	647	33	5398	5408	5418	5428	5438	5448	5458	5468	5478
5359	6665	330	5379	648	33	5399	5409	5419	5429					

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 30)

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 31)

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 32)

[illegible]

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 33)

CASE=CHNG8S SEQ= 2

PAGE 1

GENERAL HEAT TRANSFER PROGRAM, **75/12/98, *20.98.20.*

HEAT-AN*

TIME EXPENDED= 77.143 CP(SEC)

THE FOLLOWING ROUTINES ARE CALLED IN ORDER.

DVA

DVC

DSC

DVA

VCA

FLUID8

RNA

CHANGE DATA SCASEA

CHANGE DATA ICASEC

CHANGE DATA FLUID3

CHANGE DATA SEND CASE

TRANSIENT 600.

-15.

0

2000.

100.

-1.

END OF CASE REACHED ON INPUT. CARDS READ = 4

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 34)


```

**75/12/08.*20.58.23.* PAGE 2
CASE=CHNGBS SEC= 2

```

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 35)

FASTEMP

REPORT MDC A3791

MEATMAN TRANSIENT

THE FOLLOWING DATA BELONGS TO ROUTINE FLUIDR

1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100

ROUTINE FLUIDR LOADED. NCFL = 0 NCFL ACTUAL = 0

LOCATIONS USED = 833

LOCATIONS AVAILABLE = 20270

LOADING INFORMATION -11292 -11207 -10817

0075/11/00.020.58.28.0 PAGE 20 CASE= NP7 SEQ= 2

REPRODUCIBILITY OF THE
ORIGINAL PAGE IS POOR

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 36)

FASTEMP
 CASE= HP7 SEQ= 2
 PAGE 3
 0075/12/11, 020.55.24.0
 24
 K2 =
 FAHRETIME
 TIME
 24
 27
 K2 =
 FAHRETIME
 TIME
 27

FIGURE 5 - SAMPLE PROBLEM OUTPUT (SHEET 37)

FASTEMP

7. PROGRAM USAGE

Section 4 has specified the data input for a case by discussing the several types of data required. This section includes several additional requirements and general suggestions for usage of the program. The section on data input also discusses errors in the input data as it is sorted and read. This section discusses additional errors which may occur and what the computer program does in response to these errors.

7.1 MISCELLANEOUS REQUIREMENTS FOR PROGRAM USE

The (1, 10, 1) curve (calculation interval) and the (1, 10, 2) curve (output interval) are required for every case. An error is counted if these curves are omitted from the data input. (See paragraph 7.2 for an explanation of the procedure the computer program takes when a case contains errors.)

Subroutine CURVES is used to perform table lookups on curves not specified on heat transfer method subroutine data input cards and to set up arguments which may be used for table lookups in curves specified in the heat transfer method subroutines. An example of this application is the altitude versus time and velocity versus time curves which are frequently used to analyze an aircraft mission. Neither of these curves are called for by the heat transfer method subroutines directly, however, the information may be needed for the computations. Subroutine CURVES must be called in Subroutine EQDAT prior to calling any subroutines which may need arguments setup. Failure to call Subroutine CURVES first will cause a value of zero to be used on the first time step and may cause a division by zero error. (All undefined argument values are zero). The curve arguments may also be setup one time step late for the remainder of the case depending on the argument used.

7.2 SOLUTION ACCURACY

Solution accuracy may be influenced by several factors which are under control of the user. The backward finite difference solution does not alter the time step input by the user. Increasing the time step tends to increase truncation errors for transient heat transfer problems. The higher the rate of change of temperature with time, the larger the error is in the computed temperature at the end of a time step. One of the causes for this is the evaluation of properties at the last known temperatures. The linearization used for T^4 in the internal radiation heat transfer subroutines also causes errors in the computed heat flux which

FASTEMP

become larger as the rate of change of temperature increases. The user should specify the time steps for a case to reflect the heating rates input for the model boundary conditions.

7.3 STEADY STATE SOLUTIONS

Cases may be set up for steady state only or a transient analysis with steady state temperatures, optionally computed at one or more problem times. Cases of the first type may be computed by omitting all heat storage subroutines and running the case for several computations (time steps). This is necessary to allow temperature dependent properties such as specified heat and conductivity, to be evaluated at the steady state temperatures since they are evaluated at the old known temperature. Some heat transfer methods (e.g. internal radiation) employ an approximation used to linearize the heat balances. These subroutines may require a few additional iterations (time steps) to reach a steady state solution. Ten time steps will produce a steady state solution in most cases with no heat storage.

Cases which combine steady state and transient portions obviously may not use the method discussed above. Heat storage terms must be included for the transient portion of the analysis and zeroed out for the steady state computations. This may be done by inputting a density curve as a function of time and specifying the density equal to zero for the time intervals when steady state temperatures are desired. The number of time steps required to reach steady state temperatures will vary as described above (size of step is immaterial).

7.4 USER ERRORS

There are two categories of user errors; those which occur before the P-phase and those which occur during the P-phase. Errors in the input data are detected and error messages output in the M and Z-phases of the program. The computer program continues to process cards, regardless of errors which are detected, until the completion of the Z-phase. The program will compute one time step in the P-phase if errors have been detected in previous data processing phases. This is done to check as much of the data input as possible and therefore minimize the number of runs which must be made to obtain a solution. There are situations where one error causes a number of other error messages to be output.

The computer program assumes values for missing or bad input data to allow one time step to be computed. A value of 1.0 is assumed for a specified curve that is missing. A value of 1.265×10^{322} is assumed for dimension table values that

FASTEMP

have not been input. The program assumes the following values if the CASEB card is not found:

NCA = 10
MPRNT = 0
NORBIT = 0
METHOD = 3

The program assumes the following values for the CASEC variables if the card is not found:

BTIME = 0.
FTIME = 2.0
TMAX = 1000
TMIN = 2.0
TEQAL = 560.
ADD2T = 0.

Additional case data values are assumed if the following errors are detected:

- (1) The value of NCA must be greater than one for all methods.
- (2) The method number must be valid; otherwise it is set to Method 3.
- (3) FTIME must be greater than BTIME; otherwise they are reversed.
- (4) TMAX must be greater than TMIN; otherwise they are reversed.
- (5) TEQAL has three options. TEQAL = 0. causes initial temperatures to be read from CASEC cards. Either too few or too many initial temperature values being input will cause an error. The additional values of initial temperature are set equal to 560°R when too few initial temperatures are input. If TEQAL is negative, final temperatures from the preceding case (if present) are used for initial temperatures for the present case. A value of 560°R is assumed for initial temperatures if there are less nodes in the previous case than in the present case. If TEQAL is greater than zero, no error checking is done.

The following user errors occur in the P-phase.

- (1) Temperatures greater than TMAX or less than TMIN cause an error to be counted and the case is terminated.
- (2) Divide checks occur when the computations result in a division by zero and may cause mode termination by the CDC computer. Input data should be checked for zero values.

A warning message is output each time a curve is extrapolated. A curve argument outside of the range of the input values for the independent variable causes a linear extrapolation using two points closest to the value desired. This message does not cause an error to be counted as the value may or may not represent an error. The user should check the extrapolated values to determine their suitability.

8. REFERENCES

1. C. E. Whitman, KBDR General Heat Transfer Program User's Manual, MDC A0613, Vol. 1, March 1973.
2. C. E. Whitman, KBDR General Heat Transfer Program User's Manual, MDC A0613, Vol. 2, September 1970.
3. G. M. Dusinberre, Heat Transfer Calculation by Finite Differences, International Textbook Company, 1961.

APPENDIX A
SUBROUTINE DESCRIPTION AND DATA SHEETS

<u>Section</u>		<u>Page</u>
A.1.0	Heat Storage Subroutines	A-3
A.2.0	Heat Conduction subroutines	A-14
A.3.0	Heat Convection Subroutines	A-43
A.4.0	Heat Radiation Subroutines	A-51
A.5.0	Heat Flux Subroutines	A-72
A.6.0	Fluid Flow Subroutines	A-80
A.7.0	Model Subroutine	A-90
A.8.0	Miscellaneous Subroutines	A-95

Curve Specification

Almost all FASTEMP subroutines require as part of their input, curves which describe material properties, source temperatures, coefficients, and other boundary conditions. Section 4.5 describes the input and use of these curves. Curves are designated using a three number system (NRELN, NTYPE, NCLAS). The following is a standard list of curve NTYPE and NCLAS.

LIST OF CURVE NTYPE & NCLAS

NTYPE	NCLAS	CURVE DESCRIPTION
1	0	Density (lb/ft ³)
2	0	Specific heat (BTU/lb°F)
3	0	Conductivity (BTU/hr-ft-°F)
4	0	Emissivity
5	0	Interface conductance (BTU/hr-ft ² -°F)
<u>TIME STEP CURVES</u>		
10	1	Delta Tau vs. Time (Seconds), NRELN = 1
10	2	Temperature printout, NRELN = 1

ATMOSPHERIC PROPERTIES

11	1	Temperature (°R)
11	2	Pressure (psia)

TRAJECTORY DATA

12	1	Altitude (ft)
12	2	Velocity (ft/sec)
12	3	Mach number
12	4	Angle of attack (degrees)

TEMPERATURE CURVES

13	1	TAW - Adiabatic wall temperature (°R)
13	2	TR - Radiation Source temperature (°R)
13	4	TP - Known temperature for conduction (°R)

MISCELLANEOUS CURVES

15	0	h-convective film coefficients (BTU/hr-ft-°F)
17	0	Shape factor curves
19	1	Fluid flow rates (lb/hr)
99	0	Heating Rate curves (BTU/hr-ft ²)
99	0	Multiplier Curve

A.1.0 Heat Storage Subroutines

Section

Page

A.1.1

SRA, SCA, SKA, SKB, SKC, SSA

A-4

FASTEMP**A.1.1 SRA, SCA, SKA, SKB, SKC, SSA**

Purpose: These subroutines will compute the heat storage terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the element volume.

Equation: The heat storage term added to the heat balance is:

$$Q = \frac{3600}{1728} \rho C_p V B (T'_{NN} - T^o_{NN}) / \Delta \tau$$

where V is the element volume (in.³).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NM	material properties curve relative number
	X, Y, Z, δ	element dimensions (in. or deg.), used to obtain V
	R ϕ , RI, RM	
	θ , ϕ_1, ϕ_2	
	B	arbitrary constant

Required Curves:

ρ - (NM, 1, 0) - density (lb_m/ft³)
 C_p - (NM, 2, 0) - specific heat at constant pressure (Btu/lb_m-°R)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines SRA, SCA and SKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	SRA	Rectangular
	SCA	Cylindrical
	SKA	Conical
	SKB	Conical
	SKC	Conical
	SSA	Spherical

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General Heat Transfer Program

SCA - Heat Storage - Cyl.

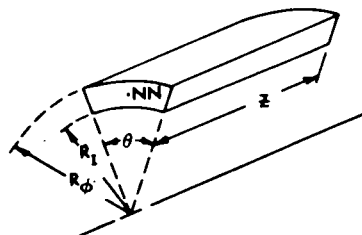
$$Q_{SCA} = \rho C \frac{\pi \theta}{P_{360}} \frac{(R_O^2 - R_I^2) Z}{1728} B (T'_{NN} - T''_{NN}) / (\Delta t / 3600)$$

NN - Node Number
R_O - Outer Radius
R_I - Inner Radius
Z - Axial Length
θ - Angle
B - Constant

Required Curves:

ρ - (NM, 1, 0) - Density

C_p - (NM, 2, 0) - Specific Heat



RCØDT		NCARD		NPRNT	NFMT														
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
SCA		0			2														

RCØDT		NCARD	NN		NM		[RØ]	[RI]	[Z]	[θ]	[B]								
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80
SCA																			

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A.2.0 Heat Conduction Subroutines

<u>Section</u>		<u>Page</u>
A.2.1	DRA, DCA, DCB, DCC, DKA, DKB, DKC, DKE, DSA, DSB, DSC (two nodes, same material)	A-15
A.2.2	DRB (two nodes or node-source/sink, two materials, interface conductance)	A-31
A.2.3	DRC, DCG, DCH, DCI (two nodes, interface conductance)	A-34

A.2.1 DRA, DCA, DCB, DCC, DKA, DKB, DKC, DKE, DSA, DSB, DSC

Purpose: These subroutines will compute the heat conduction terms between two elements of the same material. The thermal model elements may be of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the conduction geometrical shape factor.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{1}{12} k (A/L) B (T_{NP} - T_{NN})$$

where (A/L) is the element conduction geometrical shape factor (in.).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NM	thermal conductivity curve relative number
	X, Y, Z, δ	element dimensions (in. or deg.)
	R ϕ , RI, RM	
	θ, ϕ_1, ϕ_2	used to obtain (A/L)
	B	arbitrary constant

Required Curves:

k - (NM, 3, 0) - thermal conductivity (Btu/hr-ft-°R)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines DRA, DCA, DCB and DCC are also available in general format number 1.
- 2) Curve argument number 2 is available as the average temperature of the two nodes NN and NP.
- 3) The heat conduction terms are stored as two-way terms in the heat balance.
- 4) The subroutines are not valid for METH ϕ D = 7.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	DRA	Rectangular
	DCA	Cylindrical
	DCB	Cylindrical
	DCC	Cylindrical
	DKA	Conical
	DKB	Conical
	DKC	Conical
	DKE	Conical
	DSA	Spherical
	DSB	Spherical
	DSC	Spherical

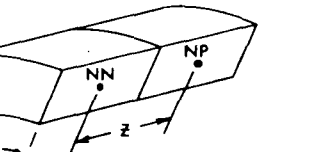
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FASTEMP	General Heat Transfer Program	DCB - Heat Conduction - Cyl., Axial
$Q_{DCB} = k \frac{\pi \theta}{360} (R\phi^2 - R_I^2) B (T_{NP} - T_{NN}) / 12Z$		
		<p> NN - Node Number NP - Node Number Rφ - Outer Radius RI - Inner Radius Z - Axial Length θ - Angle B - Constant </p>
<p>Required Curves: k - (NM,3,0) - thermal conductivity</p>		
RCODT	NCARD	NN NP NM [Rφ] [RI] [Z] [θ] [B]
1	10 14	18 22 26 30 34 38 42 46 50 54 58 62 66 70 74 78 80
DCB	0	2

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A.2.2 DRB

Purpose: This subroutine will compute the heat conduction terms between two elements or an element and a source/sink. Conduction is through two materials in a rectangular geometry with an optional interface conductance. Terms may be one-way or two-way in the heat balance.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{(B)(BB)(T_{NP} - T_{NN})}{\frac{12 X_1}{k_1 A_1} + \frac{12 X_2}{k_2 A_2} + \frac{144}{CA_{12}}}$$

Data Cards:	Symbolic Name	Value
	NN	node number of one element (if connection is one-way, flow is from this node)
	NP	node number of other element or source/sink curve relative number a) if $0 < NP \leq 4000$, NP is a node number with a two-way connection. b) if $4000 < NP \leq 5000$, (NP-4000) is the curve relative number of the source/sink temperature. c) if $NP > 5000$, (NP-5000) is a node number with a one-way connection from node NN
	NM1	thermal conductivity curve relative number for the element NN
	NM2	thermal conductivity curve relative number for the element NP
	X1	element length of node NN (in.)
	A1	element cross-sectional area of node NN (in ²)
	X2	element length of node NP (in.)
	A2	element cross-sectional area of node NP (in ²)
	A12	cross sectional area for interface conductance between node NN and NP (in ²)
	NC	interface conductance curve relative number
	B, BB	arbitrary constants

Required Curves:

k_1 - (NM₁, 3, 0) - thermal conductivity (Btu/hr-ft-°R)
 k_2 - (NM₂, 3, 0) - thermal conductivity (Btu/hr-ft-°R)
 C - (NC, 5, 0) - interface conductance (Btu/hr-ft²-°R) if NC > 0
 T_{NP} - ([NP-4000], 13, 4) - source/sink temperature (°R) if $4000 < NP \leq 5000$

Restrictions and Notes:

- 1) This subroutine is available only in general format number 2.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of k_1 ,
 - b) the temperature of node NP (or source/sink) for the evaluation of k_2 ,
 - c) the average temperature of the two nodes NN and NP (or source/sink) for the evaluation of C.
- 3) The terms B and BB may not be zero
- 4) The subroutine is not valid for METHØD = 7.

Subroutine Geometry: Rectangular

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A.2.3 DRC, DCG, DCH, DCI

Purpose: These subroutines will compute the heat conduction terms for interface conductance between two elements. The thermal model elements may be of either rectangular or cylindrical geometry. The subroutines are identical except for the interface area.

Equation: The heat conduction term added to the heat balance is:

$$Q = \frac{1}{144} C A B (T_{NP} - T_{NN})$$

where A is the interface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NC	interface conductance curve relative number
	Y, Z	element dimensions (in. or deg.)
	R ϕ , RI, θ	to obtain A
	B	arbitrary constant

Required Curves:

C - (NC, 5, 0) - interface conductance (Btu/hr-ft²-°R)

Restrictions and Notes:

- 1) All subroutines are available in general format numbers 1 and 2.
- 2) Curve argument number 2 is available as the average temperature of the two nodes NN and NP.
- 3) The heat conduction terms are stored as two-way terms in the heat balance
- 4) These subroutines are not valid for METHOD 7.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	DRC	Rectangular
	DCG	Cylindrical
	DCH	Cylindrical
	DCI	Cylindrical

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A.3.0 Heat Convection Subroutines

<u>Section</u>		<u>Page</u>
A.3.1	VRA, VCA, VKA, VSA (forced convection heat transfer coefficient, adiabatic wall temperature)	A-44

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A.3.1 VRA, VCA, VKA, VSA

Purpose: These subroutines will compute the heat convection terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry from a source/sink. The subroutines are identical except for the element surface area. Heat transfer coefficient is provided as known function.

Equation: The heat convection term added to the heat balance is:

$$Q = \frac{1}{144} h A B (T_{aw} - T_{NN})$$

where A is the element surface area (in²)

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NH	heat transfer coefficient curve relative number
	NTAW	adiabatic wall temperature curve relative number
	Y, Z RØ, RI Ø, φ ₁ , φ ₂	} element dimensions (in. or deg.)
	I	
	B	
		area option (VCA only)
		arbitrary constant

Required Curves:

h - (NH, 15, 0) - heat transfer coefficient (Btu/hr-ft²-°R)
 T_{aw} - (NTAW, 13, 1) - adiabatic wall temperature (°R)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines VRA and VKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.
- 3) These subroutines can be used to force a node to follow a prescribed temperature by letting the T_{aw} curve be the prescribed value and making the heat transfer coefficient a large number (e.g. 10⁶).

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	VRA	Rectangular
	VCA	Cylindrical
	VKA	Conical
	VSA	Spherical

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A.4.0 Heat Radiation Subroutines

<u>Section</u>		<u>Page</u>
A.4.1	RRA, RCA, RKA, RSA (external radiation, ϵF)	A-52
A.4.2	RRB (internal radiation, two gray plates)	A-59
A.4.3	RRC, RCC, RKC, RSC (internal radiation, ϵF)	A-62
A.4.4	RRD (internal radiation, enclosure)	A-69

A.4.1 RRA, RCA, RKA, RSA

Purpose: These subroutines will compute the heat radiation terms to thermal model elements of either rectangular, cylindrical, conical or spherical geometry from a source/sink. The subroutines are identical except for the element surface area.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{1}{144} \sigma \epsilon F A B (T_r^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant (0.1714×10^{-8} Btu/hr-ft²-°R⁴) and A is the element surface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NF	shape factor curve relative number from node NN to source/sink
	NM	emissivity curve relative number
	NTR	radiation source/sink temperature curve relative number
	Y, Z	} element dimensions (in. or deg.)
	RØ, RI	
	Ø, ϕ_1 , ϕ_2	
	I	
	B	area option (RCA only)
		arbitrary constant

Required Curves:

F - (NF, 17, 0) - shape factor (-)
 ϵ - (NM, 4, 0) - emissivity (-)
 Tr - (NTR, 13, 2) - radiation source/sink temperature (°R)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines RRA and RKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.
- 3) These subroutines are not valid for METHOD = 5.
- 4) Approximations are made for T^4 in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximation is exact.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	RRA	Rectangular
	RCA	Cylindrical
	RKA	Conical
	RSA	Spherical

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A.4.2 RRB

Purpose: This subroutine will compute the heat radiation terms between two thermal model elements of rectangular geometry. The radiation shape factor is computed for two gray infinite parallel plates.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{\frac{1}{144} \sigma Y Z B (T_{NP}^4 - T_{NN}^4)}{(\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1)}$$

where σ is the Stefan-Boltzmann constant
(0.1714×10^{-8} Btu/hr-ft² - °R⁴).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one node
	NP	node number of other node
	NM1	emissivity curve relative number of node NN
	NM2	emissivity curve relative number of node NP
	Y, Z	element dimensions (in.)
	B	arbitrary constant

Required Curves:

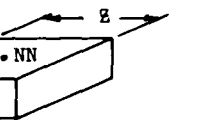
- ϵ_1 - (NM1, 4, 0) - emissivity (-)
- ϵ_2 - (NM2, 4, 0) - emissivity (-)

Restrictions and Notes:

- 1) This subroutine is available in general format numbers 1 and 2.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of ϵ_1 ,
 - b) the temperature of node NP for the evaluation of ϵ_2 .
- 3) This subroutine is not valid for METHOD = 5, 7.
- 4) Approximations are made for T^4 in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 5) The heat radiation terms are stored as two-way terms in the heat balance.

Subroutine Geometry: Rectangular

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FASTEMP	General Heat Transfer Program	RRB - Internal Radiation - Rect.																																																													
$Q_{RRB} = \sigma \left(\frac{1}{\frac{1}{\epsilon_1} + \frac{1}{\epsilon_2} - 1} \right) \frac{Y Z}{144} B (T_{NP}^4 - T_{NN}^4)$																																																															
<div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p>  </p> <p> NN - Node number NP - Node number Y } - Element Dimensions Z } B - Constant </p> </div> <div style="width: 50%;"> <p>Required curves:</p> <p> ϵ_1 - (NM1,4,0) - emissivity for node surface NN ϵ_2 - (NM2,4,0) - emissivity for node surface NP </p> <p>Note: Approximation used for T^4</p> </div> </div>																																																															
<table border="1" style="width: 100%; border-collapse: collapse; font-size: 0.8em;"> <thead> <tr> <th>RCØDT</th> <th>NCARD</th> <th>NPRNT</th> <th>NFMT</th> <th colspan="16"></th> </tr> </thead> <tbody> <tr> <td>1</td> <td>10</td> <td>14</td> <td>18</td> <td>22</td> <td>26</td> <td>30</td> <td>34</td> <td>38</td> <td>42</td> <td>46</td> <td>50</td> <td>54</td> <td>58</td> <td>62</td> <td>66</td> <td>70</td> <td>74</td> <td>78</td> <td>80</td> </tr> <tr> <td>RRB</td> <td></td> <td>0</td> <td></td> <td></td> <td>2</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table>			RCØDT	NCARD	NPRNT	NFMT																	1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	RRB		0			2															
RCØDT	NCARD	NPRNT	NFMT																																																												
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80																																												
RRB		0			2																																																										
<table border="1" style="width: 100%; border-collapse: collapse; font-size: 0.8em;"> <thead> <tr> <th>RCØDT</th> <th>NCARD</th> <th>NN</th> <th>NP</th> <th>NM1</th> <th>NM2</th> <th>[Y]</th> <th>[Z]</th> <th>[B]</th> <th colspan="12"></th> </tr> </thead> <tbody> <tr> <td>1</td> <td>10</td> <td>14</td> <td>18</td> <td>22</td> <td>26</td> <td>30</td> <td>34</td> <td>38</td> <td>42</td> <td>46</td> <td>50</td> <td>54</td> <td>58</td> <td>62</td> <td>66</td> <td>70</td> <td>74</td> <td>78</td> <td>80</td> </tr> <tr> <td>RRB</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table>			RCØDT	NCARD	NN	NP	NM1	NM2	[Y]	[Z]	[B]													1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	RRB																			
RCØDT	NCARD	NN	NP	NM1	NM2	[Y]	[Z]	[B]																																																							
1	10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80																																												
RRB																																																															

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A.4.3 RRC, RCC, RKC, RSC

Purpose: These subroutines will compute the heat radiation terms between thermal model elements of either rectangular, cylindrical, conical or spherical geometry. The subroutines are identical except for the element surface area.

Equation: The heat radiation term added to the heat balance is:

$$Q = \frac{1}{144} \sigma \epsilon F A B (T_{NP}^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant (0.1714×10^{-8} Btu/hr - ft² - °R⁴) and A is the element surface area (in²).

<u>Data Cards:</u>	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number of one element
	NP	node number of other element
	NM	emissivity curve relative number
	NFA	shape factor curve relative number from node NN to node NP
	Y, Z	element dimensions of node NN (in. or deg.)
	RØ, RI	
	Ø, Ø ₁ , Ø ₂	
	I	area option (RCC only)
	B	arbitrary constant

Required Curves:

ε - (NM, 4, 0) - emissivity (-)
F - (NFA, 17, 0) - shape factor (-)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines RRC and RKC are also available in general format number 1.
- 2) Curve argument number 2 is available as:
 - a) the temperature of node NN for the evaluation of ε,
 - b) the temperature of node NP for the evaluation of F.
- 3) These subroutines are not valid for METHOD = 5, 7
- 4) Approximations are made for T⁴ in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 5) The heat radiation terms are stored as two-way terms in the heat balance.

<u>Subroutine Geometry:</u>	<u>Subroutine</u>	<u>Geometry</u>
	RRC	Rectangular
	RCC	Cylindrical
	RKC	Conical
	RSC	Spherical

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A.4.4 RRD

Purpose: This subroutine will compute the heat radiation terms between a thermal model element and up to three other elements in an enclosure.

Equation: The heat radiation terms added to the heat balance are:

$$Q = \frac{1}{144} \sigma A \sum_{I=1}^3 F_{NI} (T_{NI}^4 - T_{NN}^4)$$

where σ is the Stefan-Boltzmann constant
(0.1714×10^{-8} Btu/hr - ft² - °R⁴).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	N1, N2, N3	node numbers of other surfaces (up to three)
	A	surface area of node NN (in ²)
	FN1, FN2, FN3	shape factors from node NN to node N1, N2 and N3 respectively

Required Curves:
None

Restrictions and Notes:

- 1) This subroutine is available in general format numbers 1 and 2.
- 2) This subroutine is not valid for METHOD = 5,7.
- 3) Approximations are made for T⁴ in order to retain a linear set of equations. These approximations are given in Appendix B. These approximations require that the temperature change of the radiation nodes remain small over the transient time steps. For steady state solutions the approximations are exact.
- 4) The heat radiation terms are stored as two-way terms in the heat balance.

Subroutine Geometry: Rectangular

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A.5.0 Heat Flux SubroutinesSectionPage

A.5.1 QCRA, QCCA, QCKA, QCSA
(heat flux, one multiplier)

A-73

A.5.1 QCRA, QCCA, QCKA, QCSA

Purpose: These subroutines will compute the heat flux terms for thermal model elements of either rectangular, cylindrical, conical or spherical geometry with a prescribed heat flux imposed on its surface. The subroutines are identical except for the element surface area.

Equation: The heat flux term added to the heat balance is:

$$Q = \frac{1}{144} q A P B$$

where A is the element surface area (in²).

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NN	node number
	NPER	multiplier curve relative number
	NQ	heat flux curve relative number
	Y, Z	element dimensions (in. or deg.)
	RØ, RI	
	Ø, Ø ₁ , Ø ₂	
	I	area option (QCCA only)
	B	arbitrary constant

Required Curves:

- P - (NPER, 99, 0) - multiplier (-)
- q - (NQ, 99, 0) - heat flux (Btu/hr - Ft²)

Restrictions and Notes:

- 1) All subroutines are available in general format number 2. Subroutines QCRA and QCKA are also available in general format number 1.
- 2) Curve argument number 2 is available as the temperature of node NN.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry</u>
	QCRA	Rectangular
	QCCA	Cylindrical
	QCKA	Conical
	QCSA	Spherical

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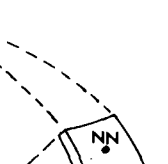
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FASTEMP	General Heat Transfer Program	QCSA - Q Curve - Sph.
$Q_{QCSA} = q \frac{\pi \theta}{180} \frac{R\phi^2}{144} (\cos \phi_1 - \cos \phi_2) PB$		
		<p>Required curves:</p> <p>P - (NPER,99,0) - Multiplier</p> <p>q - (NQ,99,0) - Heat flux</p> <p>φ₁ - Smallest latitude angle</p> <p>φ₂ - Largest latitude angle</p> <p>B - Constant</p>
RCDDT	NCARD	
1	10 14	18 22 26 30 34 38 42 46 50 54 58 62 66 70 74 78 80
QCSA	0	2
RCDDT	NCARD	NN NPER NQ [Rφ] [θ] [φ ₁] [φ ₂] [B]
1	10 14	18 22 26 30 34 38 42 46 50 54 58 62 66 70 74 78 80
QCSA		

A.6.0 Fluid Flow SubroutineSectionPage

A.6.1

FLUIDB
(fluid convection with wall heat transfer)

A-81

A.6.1 FLUIDB

Purpose: This subroutine will compute the heat terms for a fluid flowing by one or more surfaces. The fluid to wall heat transfer coefficient h may be input by the user as curve data or may be computed by the subroutine. Options are provided in the subroutine for:

- Option 0 - bulk temperature method
- Option 1 - outlet temperature method
- Option 2 - modified h method
- Option 3 - modified \dot{m} and h method

This subroutine can also be used to compute the pressure drop in the fluid control volume.

Equations: The heat terms added to the heat balance are:

$$\frac{3600}{1728} \frac{\rho C_p V B_1}{\Delta \tau} (T'_F - T_F^\circ) = Q_m + Q_w$$

where:

$$\text{Option 0} - Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} (T'_{NW} - T'_F)$$

$$T_F = 1/2 (T_{NI} + T_{N\emptyset})$$

$$\text{Option 1} - Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} (T'_{NW} - T'_F)$$

$$T_F = T_{N\emptyset}$$

$$\text{Option 2} - \beta = (\Sigma \frac{hA B_2}{144}) / \dot{m} C_p B_3$$

$$Q_m = \dot{m} C_p B_3 (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} [(e^\beta - 1)/\beta] (T'_{NW} - T'_F)$$

$$T_F = T_{N\emptyset}$$

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$$\text{Option 3} - \beta = (\Sigma \frac{hA B_2}{144}) / \dot{m} C_p B_3$$

$$C = \frac{e^\beta - \beta - 1}{\beta(e^\beta - 1)}$$

$$Q_m = \dot{m} C_p B_3 (\beta [(1 - C)/(e^\beta - 1)]) (T'_{NI} - T'_{N\emptyset})$$

$$Q_w = \frac{hA B_2}{144} [T'_{NW} - C T'_{NI} - (1 - C) T'_{N\emptyset}]$$

$$T_F = T_{N\emptyset}$$

The fluid element control volume equation options are:

user specified

$$V = X1$$

rectangular

$$V = X1 \cdot X2 \cdot X3$$

cylindrical

$$V = \frac{\pi}{4} \cdot X2^2 \cdot X1$$

If the fluid to wall heat transfer coefficient is computed by the subroutine, the equivalent diameter, D_e , and the cross sectional area, A_c , options are:

user specified

$$D_e = X2$$

$$A_c = X3$$

rectangular

$$D_e = \frac{2 \cdot X2 \cdot X3}{X2 + X3}$$

$$A_c = X2 \cdot X3$$

cylindrical

$$D_e = X2$$

$$A_c = \frac{\pi}{4} \cdot X2^2$$

The wall area equation options are:

user specified

$$A = X4$$

rectangular

$$A = X4 \cdot X5$$

cylindrical

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$$A = \pi \cdot X4 \cdot X5$$

If the curve relative number IH is not zero, the heat transfer coefficient must be input by the user as curve data. If IH is zero, the heat transfer coefficient will be computed by the subroutine according to the relations

$$Nu = C_{LAM} \cdot Re^{EXL1} \cdot Pr^{EXL2} \cdot \left(\frac{D_e}{L_o}\right)^{EXL3} \cdot \left(\frac{\mu_b}{\mu_w}\right)^{EXL4}$$

for the laminar case when $Re \leq Re_{CL}$;

$$Nu = C_{TURB} \cdot Re^{EXT1} \cdot Pr^{EXT2} \cdot \left(\frac{D_e}{L_o}\right)^{EXT3} \cdot \left(\frac{\mu_b}{\mu_w}\right)^{EXT4}$$

for the turbulent case when $Re \geq Re_{CT}$;

Nu = logarithmic interpolation between the laminar Nusselt number evaluated at Re_{CL} and the turbulent Nusselt number evaluated at Re_{CT} .

when $Re_{CL} < Re < Re_{CT}$, where:

$$Nu = \text{Nusselt Number} = \frac{h D_e}{12 k_b}$$

$$Re = \text{Reynolds number} = \frac{\rho_b V_b D_e}{\mu_b} = \frac{12 \dot{m} D_e}{3600 \mu_b A_c}$$

$$Pr = \text{Prandtl Number} = \frac{3600 C_{p_b} \mu_b}{k_b}$$

b and w denote properties evaluated at the bulk fluid and wall temperatures, respectively.

If the user specifies a value for ILC in the subroutine zero card, the constant and exponents for the laminar Nusselt number equation are obtained from the dimension table as follows:

C_{LAM} = value in dimension table location ILC
 $EXL1$ = value in dimension table location ILC+1
 $EXL2$ = value in dimension table location ILC+2
 $EXL3$ = value in dimension table location ILC+3
 $EXL4$ = value in dimension table location ILC+4

If ILC is zero or is not specified, the following default values

will be used in the laminar equation:

$$\begin{aligned}C_{\text{LAM}} &= 1.86 \\ \text{EXL1} &= 0.3333333 \\ \text{EXL2} &= 0.3333333 \\ \text{EXL3} &= 0.3333333 \\ \text{EXL4} &= 0.140\end{aligned}$$

If the user specifies a value for ITC in the subroutine zero card, the constant and exponents for the turbulent Nusselt number equation are obtained from the dimension table as follows:

$$\begin{aligned}C_{\text{TURB}} &= \text{value in dimension table location ITC} \\ \text{EXT1} &= \text{value in dimension table location ITC+1} \\ \text{EXT2} &= \text{value in dimension table location ITC+2} \\ \text{EXT3} &= \text{value in dimension table location ITC+3} \\ \text{EXT4} &= \text{value in dimension table location ITC+4}\end{aligned}$$

If ITC is zero or is not specified, the following default values will be used in the turbulent equation:

$$\begin{aligned}C_{\text{TURB}} &= 0.0225 \\ \text{EXT1} &= 0.80 \\ \text{EXT2} &= 0.3333333 \\ \text{EXT3} &= 0.0 \\ \text{EXT4} &= 0.140\end{aligned}$$

If the user specifies a value for IF in the subroutine zero card, the pressure drop in the fluid control volume will be computed.

The equation is:

$$\Delta P = \frac{1}{144} \left(\frac{4fL}{D_e} \right) \frac{(\dot{m}/3600)^2}{2 g_c \rho (A_c/144)^2} \quad \text{psi}$$

$$P_{\text{out}} = P_{\text{in}} - \Delta P$$

where:

f = friction factor input as a curve versus Reynolds number
(curve argument 30)

L = X1 variable

The inlet pressure is optional and is obtained from the card 1 type. If the inlet pressure is specified, the outlet pressure

FASTEMP

replaces it allowing the pressure through a series of control volumes to be computed. The inlet pressure to the first control volume can be specified by the MØPA subroutine.

If the pressure drop option is specified, the following printout is obtained for each fluid control volume at the print times specified by curve 1, 10, 2.

FLUIDB NI NØ ΔP P_{out} Re Nu f

(The Nusselt number is without the viscosity factor,
which is dependent on each wall section.)

<u>Data Cards:</u>	<u>Symbolic Name</u>	<u>Value</u>
	NCFØL	number of cards to follow
	IFM	fluid method
		= 0 bulk temperature method
		= 1 outlet temperature method
		= 2 modified h method
		= 3 modified \dot{m} and h method
	RECL	critical Reynolds number for laminar flow
	RECT	critical Reynolds number for turbulent flow
	ILC	index for laminar Nusselt number constants or zero
	ITC	index for turbulent Nusselt number constants or zero
	IF	friction factor curve relative number or zero
Card 1	LC	last card in control volume
		= 0 no
		= 1 yes
	NI	fluid inlet node number
	NØ	fluid outlet node number
	IFP	fluid property curve relative number
	IMD	mass flow rate curve relative number
	IGV	control volume geometry option

= -1 user specified
 = 0 rectangular
 = 1 cylindrical
 B1 volume term multiplier
 X1 }
 X2 } element dimensions for volume
 X3 }
 XLØ flow development length
 B3 flow term multiplier
 PIN control volume inlet pressure if IF \neq 0
 Card 2 LC last card in control volume
 = 0 no
 = 1 yes
 NW wall node number
 IH wall heat transfer coefficient curve
 relative number or zero
 IGA area geometry option
 = -1 user specified
 = 0 rectangular
 = 1 cylindrical
 B2 area term multiplier
 X4 }
 X5 } element dimensions for area
 Required Curves:
 f - (IF, 27, 0) - friction factor if IF \neq 0
 ρ - ($|IFP|$, 1, 0) - fluid density (lb/ft^3) if IFP $>$ 0
 R - ($|IFP|$, 1, 1) - gas constant ($\text{ft}\cdot\text{lb}_f/\text{lb}_m - ^\circ\text{R}$) if IFP $<$ 0
 C_p - ($|IFP|$, 2, 0) - fluid specific heat ($\text{Btu}/\text{lb}_m - ^\circ\text{R}$)
 k - ($|IFP|$, 3, 0) - fluid thermal conductivity ($\text{Btu}/\text{hr}\cdot\text{ft}\cdot^\circ\text{R}$)
 if IH = 0
 μ - ($|IFP|$, 8, 0) - fluid viscosity ($\text{lb}_m/\text{ft}\cdot\text{sec}$) if IH = 0
 \dot{m} - (IMD, 19, 1) - fluid mass flow rate (lb_m/hr)
 h - (IH, 15, 2) - wall heat transfer coefficient ($\text{Btu}/\text{hr}\cdot\text{ft}^2\cdot^\circ\text{R}$)
 if IH \neq 0

Restrictions and Notes:

- 1) This subroutine is only available in general format 2.
- 2) Curve argument number 2 is available as the bulk fluid temperature $T_B = 1/2 (T_{NI} + T_{NØ})$. For evaluation of μ_w ,

FASTEMP

- curve argument number 2 is available as the wall temperature T_{NW} .
- 3) If the pressure drop option is used, curve argument number 30 is available as the Reynolds number for the fluid control volume.
 - 4) For $IFP < 0$, fluid density is computed using the equation $\rho = P/RT_B$. Pressure is obtained from curve argument number 12.
 - 5) This subroutine is not valid for $METHOD = 1, 2, 5, 7$.
 - 6) The finite difference method may be unstable if the bulk temperature method ($IFM = 0$) is used. The other methods ($IFM = 1, 2, 3$) are always stable.
 - 7) Data cards are input in groups for each control volume. A fluid element card (Card 1) must be input as the first card for each control volume. These are followed by as many wall element cards (Card 2) as required. The last wall element card for a control volume must contain a 1 in column 18 to indicate the end of that control volume.
 - 8) The C_p in the heat storage term is valid for a liquid flow or a constant pressure gas flow. For a variable pressure gas flow the C_p should be changed to C_v . This can be approximated by the input of B_1 as C_v/C_p . However, in many cases the heat storage term will be negligible compared to the other terms, and can be neglected, i.e., input B_1 as zero.
 - 9) The expressions for fluid methods 2 and 3 are based on an analytical solution with negligible heat storage term. Fluid method 3 is for any number of wall nodes, fluid method 2 is for only one wall node per control volume. Fluid method 1 is valid when most of the fluid in the control is near the fluid outlet temperature, i.e., when $hA > \dot{m} C_p$. Fluid method 0 is valid when the fluid in the control volume is near an average between the fluid inlet and outlet, i.e., when $\dot{m} C_p > hA$. Fluid method 0 will be unstable if $hA > \dot{m} C_p$. Fluid method 1, 2, and 3 are always stable.

- 10) If no value is specified for the number of cards to follow, NCFØL, the subroutine assumes that 100 cards of card type 1 will be input. This value is used to allocate core storage. If multiple calls to this subroutine are made within a case, or if the number of data cards is less than the assumed number of 100, the user can reduce core storage requirements by specifying a value for NCFØL. For the purpose of this estimate, three cards of card type 2 are equivalent in data storage requirements to one card of card type 1. For example, if four cards of type 1 are input and twelve cards of type 2 are input, the value of NCFØL is equal to $(4 + 12/3)$ and is input as 8.

FASTEMP		General Heat Transfer Program										FLUIDB - Fluid flow									
		$\rho C_p \frac{V}{1728} B_1 (T_F' - T_F^O) / (\Delta\tau / 3600) = Q_m + Q_w$										XLØ - flow development length B3 - flow term multiplier PIN - optional control volume inlet pressure NW - wall node IGA - area geometry option = -1 user specified A=X4 = 0 rectangular A=X4·X5 = 1 cylindrical A=π·X4·X5 B2 - area term multiplier X4 } - element dimensions for area X5 } Required curves: if IF≠0 f - (IF,27,0) - friction factor if IFP>0 ρ - (IFP,1,0) - fluid density if IFP<0 R - (IFP ,1,1) - gas constant C - (IFP ,2,0) - fluid specific heat m ^P - (IMD,19,1) - fluid mass flow rate if IH=0 k - (IFP ,3,0) - fluid thermal conductivity μ - (IFP ,8,0) - fluid viscosity if IH≠0 h - (IH,15,2) - wall heat transfer coefficient Note: Not valid for method - 1,2,5,7									
NCFØL - number of cards to follow IFM - fluid method =0 bulk temperature method =1 outlet temperature method =2 modified h method =3 modified m and h method RECL - laminar critical Re RECT - turbulent critical Re ILC - index for laminar Nu constants ITC - index for turbulent Nu constants LC - last card in control volume =0 no =1 yes NI - inlet fluid node NØ - outlet fluid node IGV - volume geometry option = -1 user specified V = X1 = 0 rectangular V = X1·X2·X3 = 1 cylindrical V = π/4·X2 ² ·X1 B1 - volume term multiplier X1 } X2 } - element dimensions for volume X3 }																					
RCØDT		NCARD	NCFØL	NPRNT	NFMT		IFM	[RECL]	[RECT]	ILC	ITC									IF	
1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
FLUIDB		0				2															
RCØDT		NCARD	LC	NI	NØ	IFP	IMD	IGV	[B1]	[X1]	[X2]	[X3]	[XLØ]	[B3]						[PIN]	
1 Card 1		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
RCØDT		NCARD	LC	NW	IH			IGA	[B2]	[X4]	[X5]										
1 Card 2		10	14	18	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80	
FLUIDB																					

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A.7.0 Model SubroutineSectionPage

A.7.1 ØNEDMR
 (one dimensional models)

A-91

A.7.1 ØNEDMR

Purpose: This subroutine will compute the heat storage terms and the heat conduction terms for a one-dimensional thermal model composed of rectangular elements.

Equation: The heat storage terms added to the heat balance are:

$$Q = \frac{3600}{1728} \rho C_p V_i B (T_i' - T_i^0) / \Delta \tau$$

where $i = N1$ to $N2$

For each rectangular element:

$$\begin{aligned} V_i &= X Y Z / 2 / (N2 - N1) \text{ for } i = N1 \text{ or } N2 \\ &= X Y Z / (N2 - N1) \text{ for } i \neq N1 \text{ or } N2 \\ &= X Y Z \text{ for } i \text{ when } N1 = N2 \end{aligned}$$

The heat conduction terms added to the heat balance, if $N1 \neq N2$, are:

$$Q = K B (T_{i+1} - T_i)$$

where $i = N1$ to $(N2 - 1)$.

For a rectangular model:

$$K = k Y Z / 12 \Delta X_i$$

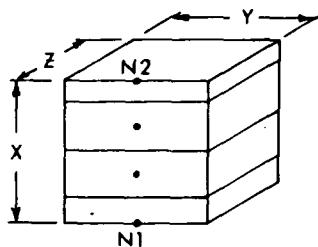
where $\Delta X_i = X / (N2 - N1)$

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	ID	directional option for ØNEDMC
	N1	node number of first element
	N2	node number of last element
	NM	material properties curve relative numbers
	X, Y, Z	element dimensions (in)
	B	arbitrary constant

Required Curves: ρ - (NM, 1, 0) - density (lbm/ft³)
 C_p - (NM, 2, 0) - specific heat at constant pressure (Btu/lbm - °R)
 k - (NM, 3, 0) - thermal conductivity (Btu/hr-ft-°R) if $N1 \neq N2$

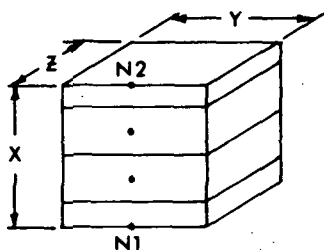
- Restrictions and Notes:
- 1) This subroutine is available in general format numbers 1 and 2.
 - 2) Curve argument number 2 is available as:
 - a) the temperature of each node for the evaluation of the density and specific heat
 - b) the average temperature of each connected node pair for the evaluation of the thermal conductivity.
 - 3) The heat conduction terms are stored as two way terms in the heat balance.
 - 4) This subroutine is not valid for METHOD = 7 if $N1 \neq N2$.
 - 5) Care must be taken if this subroutine is used with the nonsequential node number option.

Subroutine Geometry:	<u>Subroutine</u>	<u>Geometry Type</u>
	ØNEDMR	Rectangular



Required Curves:
 ρ - (NM,1,0) - Density
 C_p - (NM,2,0) - Specific Heat
 k - (NM,3,0) - Thermal Conductivity

[illegible]



Required Curves:
 ρ - (NM,1,0) - Density
 C_p - (NM,2,0) - Specific Heat
 k - (NM,3,0) - Thermal Conductivity

Note: May cause node number/equation number conflict if using nonsequential node number option.

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A.8.0 Miscellaneous Subroutines

<u>Section</u>		<u>Page</u>
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A.8.2	MOPA (miscellaneous operations, subroutine)	A-98

FASTEMP**A.8.1 CURVES**

Purpose: This subroutine allows the user to store curve argument values from the result of a table lookup from a curve.

Data Cards:	<u>Symbolic Name</u>	<u>Value</u>
	NREL	Curve relative number, type and class
	NTYPE	to be searched
	NCLAS	
	NARG	Curve argument number to store result

Required Curves: As specified by NREL, NTYPE and NCLAS

Restrictions and Notes:

- 1) The subroutine CURVE is designed for general use.
- 2) This subroutine must be called before any other subroutine which expects to use its results.
- 3) The value of NARG is ignored if the type and class of the curve matches the atmosphere/trajectory identifications shown on the data sheets.
- 4) If a velocity curve is specified (__, 12, 2), the sub-routines will also compute and store the Mach number.
If a Mach number curve is specified (__, 12, 3), the sub-routines will also compute and store the velocity.

FASTEMP		General Heat Transfer Program					CURVES - Curve Argument Loading														
<div style="display: flex; justify-content: space-between;"> <div style="width: 30%;"> <p>-,12,1 - Altitude (arg. 3)</p> <p>-,11,1 - Freestream temp. (arg.8)</p> <p>-,11,2 - Freestream pres. (arg.7)</p> <p>-,12,2 - Velocity (arg.4)</p> <p>-,12,3 - Mach number (arg.5)</p> <p>-,12,4 - Angle of attack (arg.6)</p> <p>-,11,3 - Freestream den. (arg.9)</p> </div> <div style="width: 35%;"> <p>NARG - Curve argument location to store value obtained from curve.</p> <p>If velocity specified, Mach no. will be computed $M_\infty = V_\infty / 49.1 \sqrt{T_\infty}$</p> <p>If Mach no. specified velocity will be computed $V_\infty = 49.1 \sqrt{T_\infty} M_\infty$</p> </div> <div style="width: 30%;"> <p>Required curves: - (NREL, NTYPE, NCLAS) as specified</p> <p>Note: Curve order may be important The curves shown will be automatically stored in their proper curve argument.</p> </div> </div>																					
RCDDT		NCARD		NPRNT	NFMT																
1		10 14		18 22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
CURVES		0																			
RCDDT		NCARD	NREL	NTYPE	NCLAS	NARG															
1		10 14	13	22	26	30	34	38	42	46	50	54	58	62	66	70	74	78	80		
CURVES		1		12	1																
		2		11	1																
		3		11	2																
		4		12	2																
		5		12	3																
		6		12	4																
		7		11	3																

FASTEMP

A.8.2 MØPA

Purpose: This subroutine allows the user to perform miscellaneous operations for the computation and modification of dimension table values, curve argument values, and curve values.

Equation: The result of the miscellaneous operation, R, is computed from one or two variables (V1 and V2)

$$R = f(V1, V2)$$

depending on the operation code, IØPR. The options are:

<u>IØPR</u>	<u>Result</u>
0	$R = V1$
+1	$R = V1 + V2$
+2	$R = V1 - V2$
+3	$R = V1 \times V2$
+4	$R = V1 \div V2$
+5	$R = \text{minimum}(V1, V2)$
+6	$R = \text{maximum}(V1, V2)$
+7	$R = V1 V2$
+8	$R = \text{average}(V1, V2)$
+9	$R = \begin{cases} -1.0 & \text{if } V1 < V2 \\ 0.0 & \text{if } V1 = V2 \\ +1.0 & \text{if } V1 > V2 \end{cases}$
-1	$R = V1 $
-2	$R = \sqrt{V1}$
-3	$R = \log V1$
-4	$R = \ln V1$
-5	$R = 10^{V1}$
-6	$R = e^{V1}$

Note that when the operation code is positive two variables are used to compute the result, otherwise only one variable is used. The two variables can be either dimension table values, curve argument values, or the result of a curve lookup. The result can be either a dimension table value, a curve argument value, or can be stored as a one dimensional curve value for later lookup.

An option code, IØPT, is also provided to specify when the operation is performed. When the option code is zero, the operation is performed on all time steps. When the option code is +1, the operation is performed only during the first time step.

FASTEMP

Data Cards:

<u>Symbolic Name</u>	<u>Value</u>
IRT	result type = +1 dimension table value = 0 curve argument value = -1 one dimensional curve value
IRN	result number if IRT = +1, dimension table index if IRT = 0, curve argument number if IRT = -1, curve relative number
IRC	additional result number for curve (IRT = -1 only) four digit code, ttcc, giving the curve type (tt) and class (cc)
IVIT	variable one type = +1 dimension table value = 0 curve argument value = -1 curve lookup value
IVIN	variable one number if IRT = +1, dimension table index if IRT = 0, curve argument number if IRT = -1, curve relative number
IVIC	additional result number for curve (IVIT = -1 only) four digit code, ttcc, giving the curve type (tt) and class (cc)
IØPR	operation code
IV2T	variable two type (see IVIT)
IV2N	variable two number (see IVIN)
IV2C	additional variable two number (see IVIC)
IØPT	option code

Required Curves:

As required by the result and variable type codes.

Restrictions and Notes:

- 1) This subroutine is available only in general format number 2.
- 2) This subroutine must be called before any subroutine which expects to use its results.
- 3) This subroutines dynamically uses the dimension table for all variables and results, i.e., the required dimension table values are obtained from or stored in the dimension table every time step.
- 4) Although this subroutine may store dimension table values, these values may only be referenced by this subroutine or other subroutines which dynamically use the dimension table.

3.

1

SUBROUTINE INDEX

<u>SUBROUTINE</u>	<u>SECTION</u>	<u>SUBROUTINE</u>	<u>SECTION</u>
CURVES	A.8.1	RCA	A.4.1
DCA	A.2.1	RCC	A.4.3
DCB	A.2.1	RKA	A.4.1
DCC	A.2.1	RKC	A.4.3
DCG	A.2.3	RRA	A.4.1
DCH	A.2.3	RRE	A.4.2
DCI	A.2.3	RRC	A.4.3
DKA	A.2.1	RRD	A.4.4
DKB	A.2.1	RSA	A.4.1
DKC	A.2.1	RSC	A.4.3
DKE	A.2.1		
DRA	A.2.1	SCA	A.1.1
DRB	A.2.2	SKA	A.1.1
DRC	A.2.3	SKB	A.1.1
DRD	A.2.4	SKC	A.1.1
DSA	A.2.1	SRA	A.1.1
DSB	A.2.1	SSA	A.1.1
DSC	A.2.1		
		VCA	A.3.1
FLUIDB	A.6.1	VKA	A.3.1
		VRA	A.3.1
MOPA	A.8.2	VSA	A.3.1
ONEDMR	A.7.1		
QCCA	A.5.1		
QCKA	A.5.1		
QCRA	A.5.1		
QCSA	A.5.1		

APPENDIX B

Linearization Methods

The solution of a general set of nonlinear simultaneous equations is a difficult and time consuming problem. In a thermal analyzer program the heat balance equations must be setup and solved every time step. This is not practical even for a model consisting of only a few nodes. All nonlinear terms in the heat balance are, therefore, replaced by approximate linearized terms. These approximations are given below.

(1) Radiation Approximation (all radiation subroutines)

The radiation heat flux error may be written as

$$\text{error} = \frac{q_{\text{approx.}} - q_{\text{actual}}}{q_{\text{actual}}}$$

where

$$q_{\text{actual}} \propto T^4$$

For the forward finite difference method the temperature used is that at the start of a time step

$$T = T^0$$

resulting in

$$q_{\text{actual}} \propto T^{04}$$

which is a known value and requires no approximation. For the mid finite difference method the temperature used is that at average time

$$T = \frac{1}{2} (T^0 + T')$$

resulting in

$$q_{\text{actual}} \propto (T^0 + T')^4$$

If the expression is expanded in a Taylor series about the point T^0 , evaluated at the point T' , and only the linear terms in T^0 retained, the approximate radiation heat flux is given by

$$q_{\text{approx.}} \propto 3T^{03} T' - 2T^{04}$$

The radiation heat flux error may then be written as

$$\text{error} = 3 \left(\frac{T'}{T^0} - 1 \right)$$

For the backward finite difference method the temperature used is that at the end of time step

$$T = T'$$

resulting in

$$q_{\text{actual}} \propto T'^4$$

If this expression is expanded in a Taylor series about the point T^0 , evaluated at the point T' , and only the linear terms in T^0 retained, the approximate radiation heat flux is given by

$$q_{\text{approx.}} \propto 4T^{03} T' - 3T^{04}$$

The radiation heat flux error may then be written as

$$\text{error} = 4 \left(\frac{T'}{T^0} - 1 \right)$$

Figure (B-1) shows the radiation heat flux error. It is seen that the error is small only when the temperature change over a time step is small.

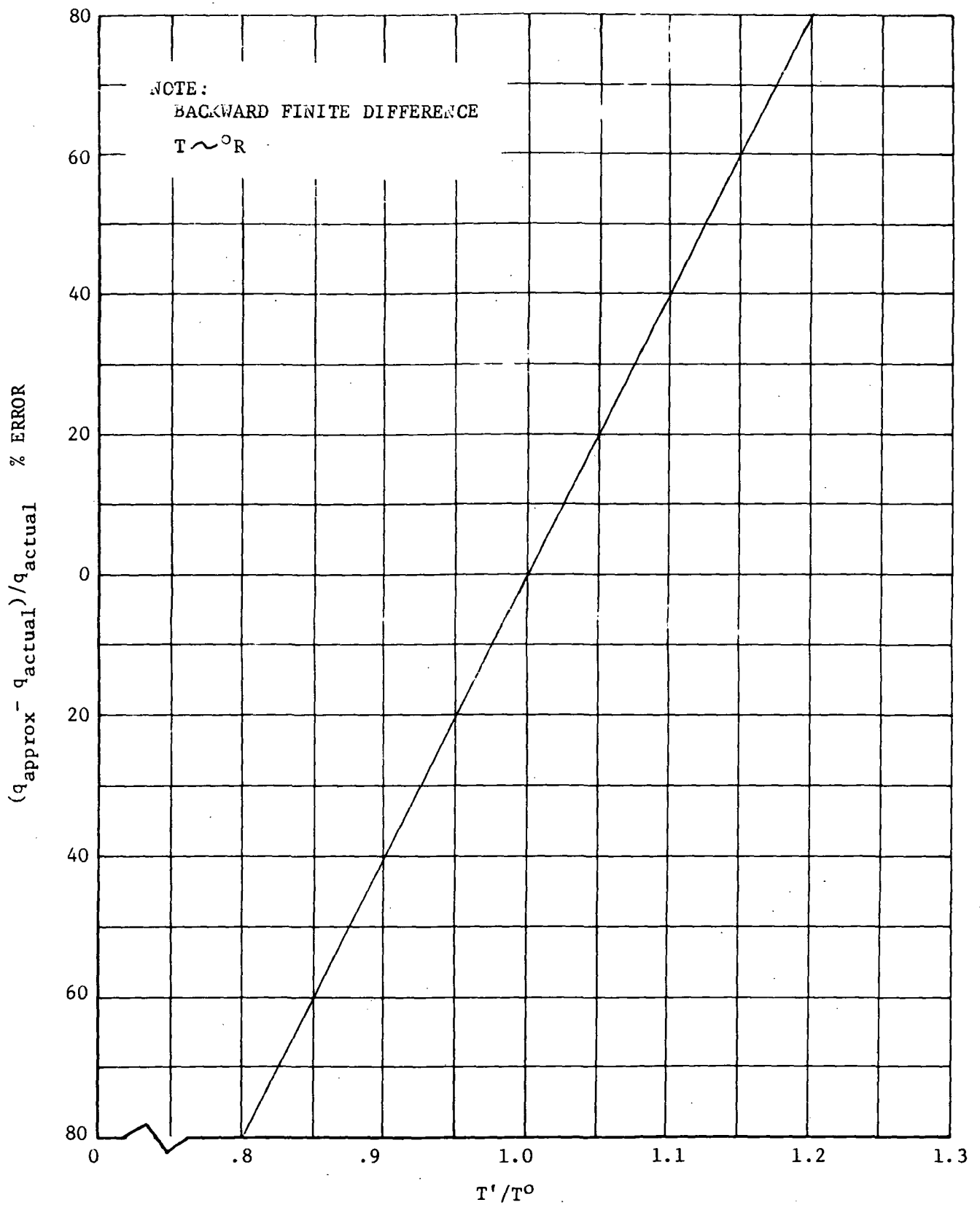


FIGURE B-1 - RADIATION APPROXIMATION ERROR

APPENDIX C
DATA INPUT FORMS

<u>Form Description</u>	<u>Page</u>
Program Specification	C-2
Case Data Input	C-3
Dimension Table Input 1	C-4
Dimension Table Input 2	C-5
Dimension Table Input 3	C-6
General Format Number 1	C-7
General Format Number 2	C-8
Temporary Curve Input 1	C-9
Temporary Curve Input 2	C-10
Same Curve Input	C-11
Case Control Cards	C-12

[illegible]

FASTEMP		GENERAL HEAT TRANSFER		CASE DATA INPUT												
NCASE - case name NCA - number of nodes MPRNT - master print control NORBIT - number of orbits METHOD - finite difference method		NSN - nonsequential node option 0 - sequential nodes 1 - nonsequential nodes														
3 - back ward (full matrix) 4 - back ward (tridiagonal matrix) 6 - back ward (K diagonal matrix) 8 - backward (Gauss-Seidel iteration)		BTIME - beginning time FTIME - final time TMAX - maximum temperature (absolute) TMIN - minimum temperature (absolute) ADD2T - value added to initial temperatures TEQAL - initial temperature option TEQAL > 0 set all to TEQAL TEQAL = 0 read in (CASET cards) TEQAL < 0 use last case answers														
1	6	7 Title				80										
CASEA																
1	6	8 NCASE 15	20 NCA	25 MPRNT	30 NORBIT	35 METHOD	40 IMP	45	50 NSN	55 ITQ	60					
CASEB																
1	6	11 BTIME	20 21	30 31 FTIME	40 41 TMAX	50 51 TMIN	60 61 TEQAL	70 71 ADD2T	80							
CASEC																
CASET																

FASTEMP			GENERAL HEAT TRANSFER		DIMENSION TABLE INPUT 1					
1	6	NPTS 10								
DIMENS										
1	6	No. 9-10	11	25	26	40	41	55	56	70
VALUES		01								
		05								
		09								
		13								
		17								
		21								
		25								
		29								
		33								
		37								
		41								
		45								
		49								
		53								
		57								
		61								
		65								
		69								
		73								
		77								
		81								
		85								

FASTEMP			GENERAL HEAT TRANSFER			DIMENSION TABLE INPUT 2				
1	6	No. 8-10	11	25	26	40	41	55	56	70
VALUES		089								
		093								
		097								
		101								
		105								
		109								
		113								
		117								
		121								
		125								
		129								
		133								
		137								
		141								
		145								
		149								
		153								
		157								
		161								
		165								
		169								
		173								
		177								
		181								
		185								

FASTEMP			GENERAL HEAT TRANSFER			DIMENSION TABLE INPUT 3				
1	6	NO. 8-10	11	25	26	40	41	55	56	70
VALUES		189								
		193								
		197								
		201								
		205								
		209								
		213								
		217								
		221								
		225								
		229								
		233								
		237								
		241								
		245								
		249								
		253								
		257								
		261								
		265								
		269								
		273								
		277								
		281								
		285								

[illegible]

[illegible]

FASTEMP					GENERAL HEAT TRANSFER					TEMPORARY CURVE INPUT 1				
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38					
TCIDNT														
1		6 7								80				
TCTITL														
		11		25 26		40 41		55 56		70				
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38					
TCIDNT														
1		6 7								80				
TCTITL														
		11		25 26		40 41		55 56		70				
1	6	NRELN 10	NTYPE 14	NCLAS 18	22	NPRNT 26	NDIMN 30	NPTS1 34	NARG1 38					
TCIDNT														
1		6 7								80				
TCTITL														
		11		25 26		40 41		55 56		70				

[illegible]

FASTEMP	GENERAL HEAT TRANSFER	CASE CONTROL CARDS
1	Cross out unnecessary cards	
END ^b CASE	Last card of each case	
BASIC	First card of each basic case (except first)	
CHANG ^b BASIC	First card of each change basic case	
CHANG ^b CHANG	First card of each change change case	
END JOB	Last card of each main subprogram data pack	